

### Test Report for an Ethylene Oxide Compliance Test at Two Sterilizers and Associated Wet Scrubber

Test Date: July 11, 2019

Long Island Sterilization Hauppauge, New York

### PREPARED FOR:

Long Island Sterilization P.O. Box 11057 175 Wireless Boulevard Hauppauge, New York 11788

### FOR SUBMITTAL TO:

New York State Department of Environmental Conservation – Region 1 Division of Air Resources 50 Circle Road Stoney Brook, New York 11790

### PREPARED BY:

ESS Group, Inc.
10 Hemingway Drive, 2nd Floor
East Providence, Rhode Island 02915

ESS Project No. L127-005.01

September 9, 2019











September 9, 2019

Ms. Nahla Babiker
Environmental Engineer
New York State Department of Environmental Conservation – Region 1
Division of Air Resources
SUNY at Stony Brook
50 Circle Road
Stony Brook, New York 11790

Re: Long Island Sterilization – Ethylene Oxide Scrubber Emissions Test – July 11, 2019

Permit ID 1-4734-00743/00006

Hauppauge, New York

ESS Project No. L127-005.01

Dear Ms. Babiker:

Enclosed for your review is one paper copy and one electronic version of our test report, dated September 9, 2019, for the ethylene oxide scrubber emission test conducted at Long Island Sterilization in Hauppauge, New York, on July 11, 2019. The results of this test demonstrate that the facility scrubber in compliance with its permit emissions limits.

Please contact me at (401) 330-1228 or <a href="mailto:epearson@essgroup.com">epearson@essgroup.com</a> if you have any questions about this report.

Sincerely,

**ESS GROUP, INC.** 

Eric A. Pearson, P.E.

Em A. Plaison

Senior Engineer

Enclosure (1 paper copy plus 1 electronic)

C: Ron Kramer, Long Island Sterilization, with enclosure (one paper and electronic)







### TEST REPORT FOR AN ETHYLENE OXIDE COMPLIANCE TEST AT TWO STERILIZERS AND ASSOCIATED WET SCRUBBER

Long Island Sterilization Hauppauge, New York

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10 Hemingway Drive, 2nd Floor East Providence, Rhode Island 02915

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### **TEST SUMMARY**

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Unit Tested:	Wet Scrubber Controlling EtO Emissions from Two Sterilizers
Test Date:	July 11, 2019
Protocol Date:	March 20, 2019



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### **1.0 INTRODUCTION**

ESS Group, Inc. (ESS) was retained by Long Island Sterilization (LIS) to perform an air emission measurement program at the LIS facility in Hauppauge, New York. The purpose of this program was to determine the ethylene oxide (EtO) removal efficiency (RE) of a Damas Corporation wet scrubber and an Anguil Environmental Systems catalytic oxidizer that control EtO emissions from two sterilizers and associated sterilization operations. The wet scrubber is the primary control device, controlling EtO emissions from the sterilizer evacuations. The oxidizer is a secondary control device operating in series with the scrubber, controlling EtO emissions from the scrubber as well as emissions from the aeration room and the vents over the sterilizer back doors.

This test program was conducted in conformance with a permit to construct (No. 1-4734-00743/00001) issued by the New York State Department of Environmental Conservation (NYSDEC). This facility uses more than 10 tons of EtO each year. Therefore, as required by the permit to construct, and in accordance with 40 CFR 63 Subpart O, the scrubber must achieve an EtO removal efficiency (RE) of 99% during the first re-evacuation of the sterilizer chamber, and the oxidizer must achieve an EtO RE of 99% or a 1 part per million outlet concentration, whichever is less stringent, during venting of the aeration room.

Testing was conducted on July 11, 2019 by Eric Pearson of ESS and CK Environmental, an ESS subcontractor. Ron Kramer of LIS coordinated the test and provided process and logistical support. Nahla Babiker of the NYSDEC was on site to observe the test program.

In consultation with the NYSDEC observer, testing was completed only on the wet scrubber due to technical issues that prevented isolation of aeration room emissions from sterilizer emissions in accordance with the planned test schedule. Testing of the oxidizer and the associated aeration room emissions is currently planned for October 2019.

Section 2.0 of this report summarizes the results of this measurement program. Section 3.0 describes the process and associated control equipment. Section 4.0 describes the test methods used, and Section 5.0 describes the quality control plan for this test program. Field data sheets, process data and other pertinent documents are included in the Appendices.

### 2.0 SUMMARY OF RESULTS

### 2.1 Sterilizer Re-Evacuation and Wet Scrubber Removal Efficiency

The scrubber EtO removal efficiency was measured during the first re-evacuation from each sterilizer over three sterilization cycles (two cycles from Sterilizer 1 and one cycle from Sterilizer 2). During these tests, the sterilizer chambers were empty. Each of the three test periods (re-evacuations) was 10 to 15 minutes in duration.

EtO emissions at the scrubber outlet were measured following the test methods described in 40 CFR 63.365 and EPA Method 25A (40 CFR 60 Appendix A). EtO emission concentrations were directly measured with a total hydrocarbon (THC) flame ionization detection (FID) analyzer calibrated with propane and EtO compressed gas standards so that the outlet concentrations are expressed as EtO. The Method 25A data were recorded on a data logger, thus yielding continuous real-time data. Gas flow rate measurements were continuously recorded during each test period using a pitot tube and manometer, following EPA Methods 1 and 2.

For each first re-evacuation, the mass of EtO loaded to the sterilizer was calculated from the pressures and temperatures of the sterilizer before and after charging. In addition, the weight loss of the EtO cylinders used to charge the sterilizer also was recorded. The residual mass of EtO in the sterilizer after the first re-evacuation was calculated from the pressures and temperatures of the sterilizer. This residual was subtracted from the EtO loaded to calculate the net mass of EtO applied to the scrubber inlet.

The scrubber efficiency measurement results are summarized in Table 2.1. Over the three test runs, the RE ranged from 99.63 to 99.75 percent, averaging 99.68 percent, well above the permit requirement of 99



percent. And, if a nominal 90 percent control efficiency is assumed for the catalytic oxidizer (operated in series with the scrubber), the actual overall EtO RE during the sterilizer re-evacuations is 99.97 percent.

As shown on Table 2.1, the calculated EtO charged to each sterilizer differed from the measured EtO charged (based on cylinder weighing) by approximately 6.7% over the three test runs. The reason for this difference is uncertain, and may reflect a combination of inherent measurement/monitoring inaccuracies. The average wet scrubber removal efficiency shown in Table 2.1 is based on the more accurate calculated EtO charged.

### 3.0 PROCESS DESCRIPTION

### 3.1 General

The LIS facility sterilizes products used in the medical industry. The facility currently operates two identical 12-pallet Environmental Techtonics EtO sterilization chambers, each with external dimensions of approximately 55 feet long x 8 feet wide x 6 feet high, and each with an internal volume of approximately 1685 cubic feet. The sterilant used in the LIS facility is 100% EtO. The evacuations from each sterilizer first pass through an acid/water scrubber manufactured by Damas Corporation. The scrubbed gas then passes through an Anguil catalytic oxidizer, which vents to the atmosphere directly through a stack approximately 60 feet above grade.

Upon completion of a sterilization cycle, product is moved from the sterilizer to a heated aeration room to allow for final degassing of EtO from the product. The air exhausted from the aeration room is combined with fugitive vent streams from the sterilization chamber areas and is vented directly to the catalytic oxidizer. A schematic of the sterilization and control equipment is shown in Figure 3.1.

### 3.2 Sterilization Process

EtO is used in this sterilization process to destroy potential infectious contaminants found on medical products. During a typical sterilization cycle, the materials to be sterilized are on pallets which are positioned at the front of the sterilizer and then drawn into the sterilizer chamber on a conveyor system. The chamber is then sealed and brought to a vacuum of approximately 45 kilo pascals (kPa) absolute. [One standard atmosphere is approximately 101 kPa.] The chamber is then washed with nitrogen to reduce the oxygen concentration, evacuated again to 45 kPa, then heated and humidified to 50 kPa with steam. When the temperature and humidity have reached specified limits, 100% EtO gas is fed into the sterilization chamber to 75 kPa, and then nitrogen is added to 90 kPa. The resulting EtO concentration within the chamber is 400 – 500 mg/L. This starts the exposure phase of the sterilization cycle. The duration of the exposure phase varies in accordance with the materials being sterilized, and typically ranges from two to six hours.

Once the exposure phase is complete, the first re-evacuation begins. The sterilization chamber is evacuated to 45 kPa over a period of approximately 30 minutes, and the evacuated gases are vented directly to the scrubber. EtO emissions from the sterilizer are at their highest during the first evacuation. Product sterilization is theoretically complete at this point of the cycle, however the product still may contain unacceptable levels of EtO.

Residual EtO within the product is then removed by a process called nitrogen washing. Nitrogen is bled into the sterilization chamber to 95 kPa and then evacuated to 45 kPa. At the LIS facility, two to four nitrogen washes are used to remove residual EtO from the product, and these washes are referred to as the second, third and fourth re-evacuations. Emissions of EtO during the washes are much less than those from the first re-evacuation. After the last re-evacuation, the chamber is filled with fresh air and flushed for about 20 minutes before being unloaded. The air flush is vented to the oxidizer through vents near the rear doors of the chamber.

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Upon completion of the sterilization cycle, the sterilized products are moved to the adjacent aeration room to allow for further off gassing of EtO. The aeration room is also vented to the catalytic oxidizer to prevent an accumulation of EtO within the room. The room is heated to approximately 110°F to increase the rate of off-gassing from the product. The sterilized materials remain in the aeration room until product residual EtO concentrations fall below the acceptable limits.

### 3.3 Damas Scrubber

A Damas Model 1000 3XP EtO scrubber (hydrolytic acid scrubber) is the primary control device in operation at the LIS facility. The scrubbing process utilizes a sulfuric acid/water solution to convert EtO to ethylene glycol (EG). The pH of the scrubber liquid is maintained below 2.5, and is continuously monitored and displayed on a digital panel meter.

Sterilizer exhaust gas is broken into small bubbles as it leaves the distribution manifold at the base of the scrubber body. EtO is absorbed by the scrubber liquid as the bubbles move toward the surface of the liquid. A fan pulls the remaining gas from the head space over the scrubber liquid, combines it with make-up air and vents the EtO/air mixture to the oxidizer. Including the make-up air, the total gas flowrate from the scrubber is approximately 300 scfm.

As the EG accumulates, the liquid volume in the scrubber vessel increases. When the liquid reaches a prescribed level (slightly lower than the maximum level), liquid is first neutralized with caustic and then pumped over to an adjacent holding tank, and fresh acid solution is added to the scrubber vessel. The liquid in the holding tank is shipped off-site for recycling.

### 3.4 Anguil Catalytic Oxidizer

The Anguil Model 30 catalytic oxidizer has a design capacity of 3000 scfm, with a design destruction efficiency of 99%, or 1 ppmv outlet concentration for dilute gas streams.

EtO laden air from the scrubber, aeration room and chamber rear vents first enters a filter plenum and then passes through a shell and tube heat exchanger which preheats the process exhaust while cooling the oxidizer exhaust. Constructed of stainless steel, it is designed for a heat transfer efficiency of approximately 65%

The preheated process exhaust stream is further heated by exposure to a gas burner which has a gross heat release capacity of 3.2 MMBtu/hour. The burner is automatically modulated to maintain a process gas temperature of at least 280°F before entering the catalyst bed for final destruction of EtO. The process gas then passes through the heat exchanger again and then through the fan and stack.

The catalyst is a manganese dioxide pellet blend, compounded and shaped by the Carus Corporation. The system fan is a variable speed unit rated at 25 HP. Flow through the oxidizer is approximately 2200 scfm, with about 300 scfm from the scrubber and 1900 scfm from the aeration room. When the sterilizer chamber rear vents are operated at the end of a sterilization cycle, the aeration room exhaust is reduced to accommodate the flow rate of the rear vents and maintain a steady flow to the oxidizer.

### 3.5 Process Operation During the Test Program

Except as noted below, the sterilizers and EtO control equipment were operated in a normal manner throughout the test program. During each sterilizer re-evacuation test period, the two sterilizers were operated with no product inside the sterilizers, though products continued to aerate in the aeration room. LIS monitored and recorded all pertinent operating parameters, including scrubber liquid level and pH. All process data are shown in Appendix B of this protocol.

The time schedule for the operation of the two sterilizers was modified in order to compress the duration of the overall sterilization cycle and allow testing to be conducted within one normal work day. The



approximate time schedule used for the operation of the sterilizers during this test program is summarized in Table 3.1.

### **4.0 SAMPLING AND ANALYSIS METHODS**

### 4.1 General

The following US EPA reference test methods were used for this test program.

- US EPA Method 1 Sampling and Velocity Traverse Points for Stationary Sources
- US EPA Method 2 Determination of Stack Gas Velocity and Volumetric Flow Rate
- US EPA Method 3A Determination of Oxygen and Carbon Dioxide Concentrations in Emissions from Stationary Sources (Instrumental Analyzer Procedure)
- US EPA Method 4 Determination of Moisture Content in Stack Gases
- US EPA Method 25A Determination of Total Organic Concentration Using a Flame Ionization Analyzer
- 40 CFR 63.365 Subpart O Ethylene Oxide Emission Standards for Sterilization Facilities

### 4.2 EtO Entering the Wet Scrubber During First Re-Evacuation

The mass of the EtO charged into the sterilizers was calculated from the chamber temperatures and pressures after charging, and the EtO cylinders used to charge the sterilizers were weighed before and after charging. Weights were recorded to the nearest 0.1 pound using calibrated scales. The residual mass of EtO remaining in the sterilizers after the first re-evacuation is calculated from the chamber temperatures and pressures immediately after the first re-evacuation. The following equations are used:

```
\label{eq:wc} \begin{aligned} \text{Wc} &= \text{EtO charged (g)} = \text{MW x F x (}\Delta\text{P/Pf) x Pf x V/(R x T)} & \text{(Equation 1)} \\ \text{Where:} & \text{MW} &= \text{Molecular weight of EtO} \\ & \text{F} &= \text{volume fraction of EtO} &= 1.00 \text{ (}100\% \text{ EtO)} \\ & \Delta\text{P} &= \text{chamber pressure increase due to the addition of EtO (kPa)} \\ & \text{Pf} &= \text{final chamber pressure before the first re-evacuation (kPa)} \\ & \text{V} &= \text{chamber volume (L)} &= 1685 \text{ ft3} &= 47,719 \text{ L} \\ & \text{T} &= \text{chamber temperature (K)} \\ & \text{R} &= \text{gas constant} &= 8.313 \text{ L-kPa/gmole-K} \\ \\ & \text{Wr} &= \text{residual EtO} &= \text{MW x F x (}\Delta\text{P/Pf) x Pa x V/(R x T)} \end{aligned} \tag{Equation 2}
```

The total mass of ethylene oxide applied to the scrubber inlet is calculated by subtracting the residual weight from the charged weight:

 $\Delta P/Pf$  = mole fraction of EtO in the chamber

 $W_i = Wc - Wr$ 

### 4.3 EtO Leaving the Scrubber and Entering and Leaving the Control Devices

The weight of ethylene oxide entering the scrubber is described above for the scrubber inlet, and the weight of ethylene oxide leaving the scrubber was determined as described in 40 CFR 63.365 and EPA Method 25A.

Concurrently with the Method 25A measurements, volumetric flow rate measurements were made at the scrubber outlet using EPA Method 2 of 40 CFR 60 Appendix A. Complete two-port traverses were made at the scrubber outlet prior to the first test run by positioning a pitot tube and manometer at the traverse

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points across the duct and measuring velocity head and temperature at each point. During each test run, the pitot was attached to an electronic pressure transducer and positioned at a single average flow point, and the velocity head and temperature were continuously measured and recorded. The static pressure was measured with a length of stainless steel tubing positioned normal to the flow and attached to a manometer which was read during each test run.

The molecular weight of the gas stream at the scrubber outlet was assumed to be 29 since it consisted primarily of ambient make-up air.

At the scrubber outlet, the total volume of gas exhausted during the test run was determined by multiplying the average measured volumetric flow rate by the total duration of each test run. The mass of EtO emitted at the scrubber outlet location was calculated using the following equation:

 $W_e = EtO \ emitted \ (g) = C \ x \ Vg \ x \ MW \ x \ 28.32/(k \ x \ 10^6)$ 

(Equation 3)

Where:

C = EtO concentration (ppmv)

Vg = volume of gas emitted during the sampling period (standard cubic feet

at 20°C and 101 kPa)

MW = molecular weight of EtO = 44 g/g-mole

k = 24.05 L/g-mole = standard molar volume at 20°C and 101 kPa

### 4.4 Sampling Locations

All sampling locations are shown in Figure 4.1. Individual locations are described below:

The scrubber outlet sampling location is in a nominal 10-inch diameter vertical duct just below the oxidizer filter plenum, approximately 2.6 duct diameters downstream from a 90-degree bend leading from the scrubber and approximately 0.6 diameters upstream from the plenum. This location is shown schematically in Figure 4.2. Initial flow rate measurements were made at 16 traverse points through two ports (8 points per port) in order to establish an average flow point. The EtO sampling probe was positioned approximately at the center of the duct.

The oxidizer inlet sampling location is in a horizontal section of a nominal 14-inch diameter duct between the heat exchanger inlet plenum on the top of the oxidizer housing and the filter plenum. This location is approximately 3.4 duct diameters downstream from a 90-degree duct bend leading from the filter plenum and approximately 3.4 duct diameters upstream from the inlet plenum. This location is shown schematically in Figure 4.3. Initial flow rate measurements were made at 16 traverse points through two ports (8 points per port) in order to establish an average flow point. The EtO sampling probe was positioned approximately at the center of the duct.

The oxidizer outlet sampling location is in the nominal 18-inch diameter vertical oxidizer stack, approximately 6.7 duct diameters downstream from the fan breeching and approximately 6.7 duct diameters upstream from the stack top. This location is shown schematically in Figure 4.4. Initial flow rate measurements were made at 16 traverse points through two ports (8 points per port) in order to establish an average flow point. The EtO sampling probe was positioned in the center of the fan exhaust transition between the fan and the stack.

### 4.5 Flow Rate Measurements

During the initial flow rate measurements prior to the first test run, a pitot tube connected to an inclined manometer was used to determine the velocity head pressure of the duct gasses at each traverse point as specified in US EPA Reference Method 2. Temperature was measured at each point with a thermocouple.

At each location during each test run, the pitot was secured at the average flow point and attached to an electronic pressure transducer. The output signals from the transducer and thermocouple was continuously



recorded on a data logger. These data were averaged over each test run to yield an average velocity pressure (delta-p) and temperature and an average flow rate. The static pressure was measured with a length of stainless steel tubing positioned normal to the flow and attached to a water manometer which was read during each test run.

### 4.6 Molecular Weight Determination

The molecular weight of the gas stream at the scrubber outlet was assumed to be 29 since it consisted primarily of ambient make-up air.

### 4.7 Moisture

The scrubber outlet moisture concentration was documented by measuring the outside air dry bulb temperature and relative humidity.

### 4.8 US EPA Methods 25A and 18

EtO emission measurements were performed following US EPA Methods 25A. The Method 25A sampling train consisted of a short, stainless-steel probe, a Teflon®, heated sample line, and a TECO Model 51i FID THC analyzer used at the scrubber outlet. A schematic of this sampling train is shown in Figure 4.5. Analyzer outputs were continuously recorded on a data logger. The analyzer was calibrated with propane compressed gas standards at three points plus zero at the beginning of the test day and at one point plus zero periodically during the test day. Concentrations were expressed as propane.

The analyzer was also calibrated with an EtO compressed gas standard to establish an EtO/propane response factor. In this way the THC data expressed as propane were also expressed as EtO in order to quantify emissions as EtO.

### 4.9 Calculation for the Scrubber Removal Efficiency

The EtO removal efficiency of the scrubber is calculated with the following equation:

E = 100 (Wv - We)/Wv

Where: E = efficiency (%)

Wv = Weight of EtO vented to the scrubber We = Weight of EtO emitted from the scrubber.

### **5.0 QUALITY CONTROL PROCEDURES**

ESS emission testing teams are committed to providing high quality testing services. To meet this commitment, applicable US EPA sampling procedures and applicable quality assurance/quality control procedures are followed with all test programs. These procedures ensure that all sampling is performed by competent, trained individuals and that all equipment used is operational and properly calibrated before and after use.

The ESS QA program generally follows the guidelines of the US EPA Quality Assurance Handbook for Air Pollution Measurement Systems: Volume III Stationary Source - Specific\_Methods (EPA-600/R-94-038c - September 1994).

### 5.1 Sampling

Measurement devices and gas analyzers are uniquely identified and calibrated with documented procedures and acceptance criteria. Records of all calibration data are maintained on file. Copies of pertinent calibration data are available on site during testing. Field data are recorded on standard forms. Field notes are used to record observations and information that may affect data quality.

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### 5.2 Analytical

Field blanks of all applicable sampling reagents are taken in accordance with the respective sampling methods. Any samples requiring off-site laboratory analysis are accompanied to the laboratory with chain-of-custody documentation. Compressed gas/calibration standards used are US EPA Protocol No. 1-certified, if applicable. Other gas standards and analytical laboratory support gases used are directly traceable to the National Institute of Standards and Technology. The certifications of the gas standards used during testing are available on site and are included in the final test report.

			Tables
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### Table 2.1 Summary of Results Sterilizer Re-Evacuation / Wet Scrubber

### Long Island Sterilization Hauppauge, NY

July 11, 2019

Wv = t V Wo dP Tc Wc Pf Pa Te Wr Wc - Wr Cp Ce Q We RE

						Pressure	Avg. Temp.	Calculated	Pressure	Pressure	Avg. Temp.		EtO	Avg. EtO	Conc. at		EtO emitted	
		Process	Elapsed	Sterilizer	EtO	Rise from	Over	EtO	Before	After	Over	Residual	Vented to	Scrubber	Outlet		from	Removal
		Clock	Time	Volume	Charged	Charging	Charging	Charged	Evac.	Evac.	Evac.	EtO	Scrubber	(ppm	ıv) <sup>d</sup>	Flow Rate	Scrubber	Efficiency
Run	Sterilizer	Time	(min)	(L)	(lbs) <sup>a</sup>	(kPa)	(°C)	(lbs) <sup>b</sup>	(kPa)	(kPa)	(°C)	(lbs) <sup>c</sup>	(lbs)	as propane	as EtO <sup>e</sup>	(scfm) <sup>f</sup>	(lbs) <sup>g</sup>	(%) <sup>h</sup>
1	1	1232-1243	11	47,719	45.6	27.0	45	47.277	90.3	48.4	45	25.340	21.937	123.4	284	209	0.075	99.66
2	2	1244-1259	15	47,719	41.8	27.0	45	47.277	90.1	48.4	45	25.396	21.881	97.6	224	209	0.080	99.63
3	1	1614-1624	10	47,719	45.8	27.0	45	47.277	90.2	48.4	45	25.368	21.909	101.1	233	210	0.056	99.75
																	Average:	99.68
																	Permit:	99

- a) Based on EtO cylinder weighing.
- b) Wc =  $(mw \times dP \times V) / [R \times (Tc + 273)] / 453.6$  where R = gas constant = 8.313 L-kPa/gmole-K
- c)  $Wr = (mw \times Pa \times (dP/Pf) \times V) / [R \times (Tc + 273)] / 453.6$  where dP/Pf is the mole fraction of EtO in the sterilizer before evacuation.
- d) parts per million, volume to volume
- e) ppmv as EtO = ppmv as propane x 2.3 (EtO/propane response factor)
- f) standard cubic feet per minute at 68°F (20°C) and 29.92 inches mercury (101 kPa)
- g) We = Ce x Q x t x mw /( k x  $10^6$ ) where k = standard molar volume = 385 ft3/lb-mole
- h) RE = 100(Wv We) / Wv

### Table 3.1 Operating Schedule for Sterilizer Scrubber Compliance Test Long Island Sterilization Hauppauge, NY

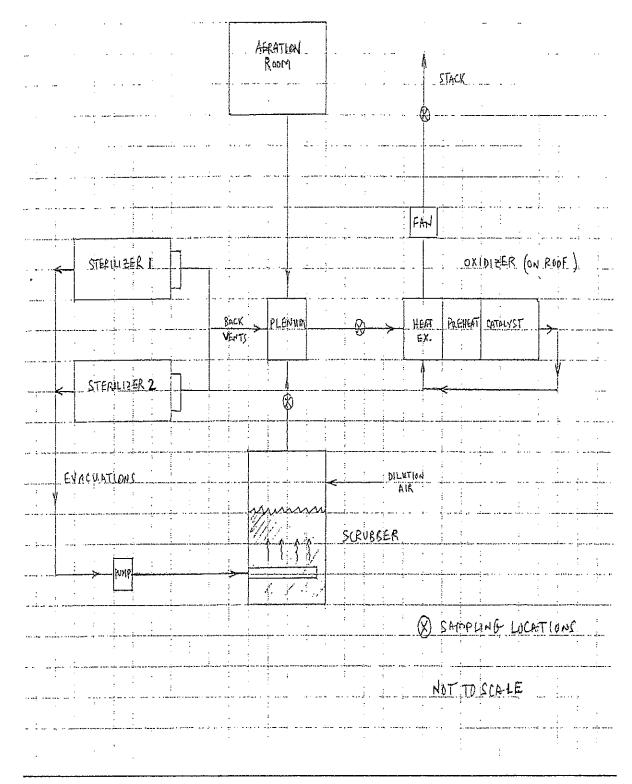
July 11, 2019

	1									
			Time		Time		Time			
Run	Sterilizer	Operation	Start	End	(min)	Comments				
	1	chamber preparation	1105	1201						
		add EtO	1201	1215						
		final preparation and hold	1215	1232						
1		1st re-evacuation	1232	1243	11					
		N2 washes and completion	1243	1446						
	2	chamber preparation	1111	1215						
		add EtO	1215	1228						
		final preparation and hold	1228	1244						
2		1st re-evacuation	1244	1259	15					
		N2 washes and completion	1259	1459						
	1	chamber preparation	1447	1543						
		add EtO	1543	1557						
		final preparation and hold	1557	1614						
3		1st re-evacuation	1614	1624	10					
		hold	1624							
	2	2	1 chamber preparation add EtO final preparation and hold 1 1st re-evacuation N2 washes and completion 2 chamber preparation add EtO final preparation and hold 2 1st re-evacuation N2 washes and completion  1 chamber preparation add EtO final preparation and hold 1 st re-evacuation  1 chamber preparation add EtO final preparation and hold 3 1st re-evacuation	Run         Sterilizer         Operation         Start           1         chamber preparation         1105           add EtO         1201         1201           final preparation and hold         1215           1         1st re-evacuation         1232           N2 washes and completion         1243           2         chamber preparation         1111           add EtO         1215           final preparation and hold         1228           2         1st re-evacuation         1244           N2 washes and completion         1259           1         chamber preparation         1447           add EtO         1543           final preparation and hold         1557           3         1st re-evacuation         1614	1 chamber preparation 1105 1201 add EtO 1201 1215 final preparation and hold 1215 1232 1243 N2 washes and completion 1243 1446	Run         Sterilizer         Operation         Start         End         (min)           1         chamber preparation         1105         1201           add EtO         1201         1215           final preparation and hold         1215         1232           1         1st re-evacuation         1232         1243         11           N2 washes and completion         1243         1446           2         chamber preparation         1111         1215         1228           4         final preparation and hold         1228         1244         1259         15           N2 washes and completion         1259         1459         15         1459         15           1         chamber preparation         1447         1543         1557         1614         1614         1624         10           3         1st re-evacuation         1614         1624         10				





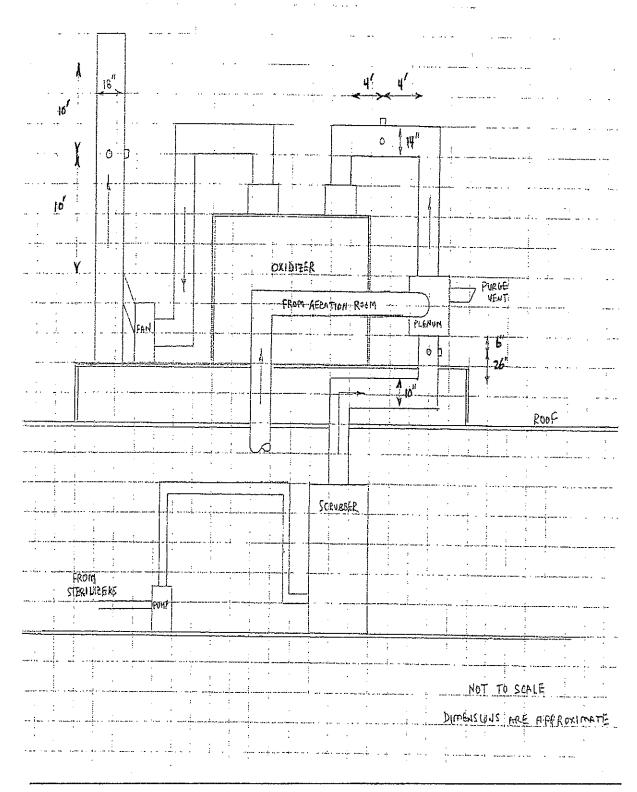






LONG ISLAND STERILIZATION HAUPPAUGE, NEW YORK

**Process and Control Equipment Schematic** 





LONG ISLAND STERILIZATION HAUPPAUGE, NEW YORK

Sampling Location Schematic



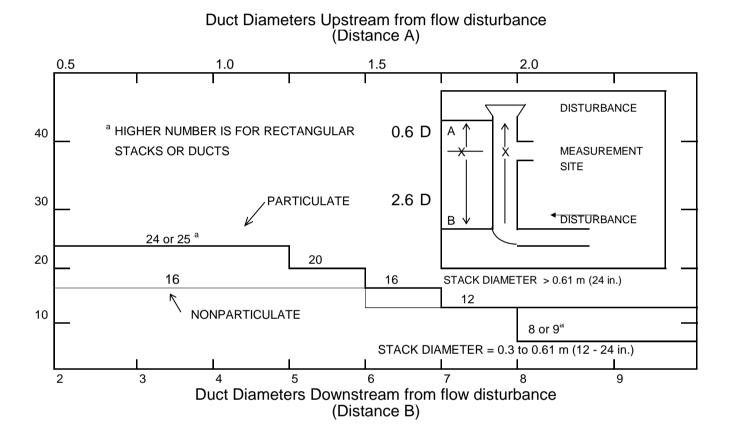
### Figure 4.2 Scrubber Outlet Sampling Location

### **Sample and Velocity Traverses for Stationary Sources**

Client	Long Island Sterilization	<b>Proj. No.</b> L127-004
Facility		
City, State	Hauppauge, NY	
Test Date		
Test Locat	ion Scrubber Outlet	
Diameter o	f Stack 9.75	inches

Diameters Upstream of Disturbance (A)	0.6
Diameters Downstream of Disturbance (B)	2.6
Total No. of Traverse Points Required	16
Number of Ports	2
Traverse Points per Port	8
Traverse (Horizontal or Vertical)	Н

### MINIMUM NUMBER OF TRAVERSE POINTS FOR PARTICULATE AND NONPARTICULATE TRAVERSES



### D W W Deq = 2LW = \_\_\_\_

9.75 inches

CROSS-SECTIONAL LAYOUT FOR RECTANGULAR STACKS				
l otal	Matrix			
Traverse Points				
9	3 x 3			
12	4 x 3			
16	4 x 4			
20	5 x 4			
25	5 x 5			

### LOCATION OF TRAVERSE POINTS IN CIRCULAR STACKS

Point Number On A Diameter	(Percent of stack diameter from inside wall to traverse point) Number of Traverse Points on a Diameter 4 6 8 10 12					
1	6.7	4.4	3.2	2.6	2.1	
2	25.0	14.6	10.5	8.2	6.7	
3	75.0	29.6	19.4	14.6	11.8	
4	93.3	70.4	32.3	22.6	17.7	
5		85.4	67.7	34.2	25.0	
6		95.6	80.6	65.8	35.6	
7			89.5	77.4	64.4	
8			96.8	85.4	75.0	
9				91.8	82.3	
10				97.4	88.2	
11					93.3	
12					97.9	

METHOD-1.xls / LGP / rev.2 - 02/97

### TRAVERSE POINT LOCATIONS

No.	Distance from Wall (inches)	Port Depth (inches)	Total Distance (inches)
1	0.5	2.5	3.0
2	1.0	2.5	3.5
3	1.9	2.5	4.4
4	3.1	2.5	5.6
5	6.6	2.5	9.1
6	7.9	2.5	10.4
7	8.7	2.5	11.2
8	9.3	2.5	11.8
9			
10			
11			
12			



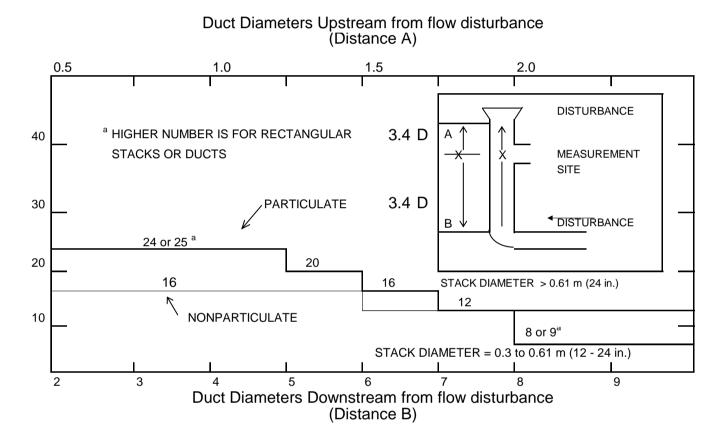
### Figure 4.3 Oxidizer Inlet Sampling Location

### **Sample and Velocity Traverses for Stationary Sources**

Client	Long Island Sterilization	<b>Proj. No.</b> L127-004
Facility		
City, State	Hauppauge, NY	
Test Date		
Test Locat	ion Oxidizer Inlet	
Diameter o	f Stack 13.25	inches

Diameters Upstream of Disturbance (A)	3.4
Diameters Downstream of Disturbance (B)	3.4
Total No. of Traverse Points Required	16
Number of Ports	2
Traverse Points per Port	8
Traverse (Horizontal or Vertical)	Н

### MINIMUM NUMBER OF TRAVERSE POINTS FOR PARTICULATE AND NONPARTICULATE TRAVERSES



## D W Deq = 2LW = \_\_\_\_

13.25 inches

CROSS-SECTIONAL LAYOUT FOR RECTANGULAR STACKS				
I otal	Matrıx			
Traverse Points				
9	3 x 3			
12	4 x 3			
16	4 x 4			
20	5 x 4			
25	5 x 5			

### LOCATION OF TRAVERSE POINTS IN CIRCULAR STACKS

Point Number On A Diameter	(Percent of stack diameter from inside wall to traverse point) Number of Traverse Points on a Diameter 4 6 8 10 12							
1	6.7	4.4	3.2	2.6	2.1			
2	25.0	14.6	10.5	8.2	6.7			
3	75.0	29.6	19.4	14.6	11.8			
4	93.3	70.4	32.3	22.6	17.7			
5		85.4	67.7	34.2	25.0			
6		95.6	80.6	65.8	35.6			
7			89.5	77.4	64.4			
8			96.8	85.4	75.0			
9				91.8	82.3			
10				97.4	88.2			
11					93.3			
12					97.9			

METHOD-1.xls / LGP / rev.2 - 02/97

### TRAVERSE POINT LOCATIONS

No.	from Wall	Port Depth	Total Distance
	(inches)	(inches)	(inches)
1	0.5	3.0	3.5
2	1.4	3.0	4.4
3	2.6	3.0	5.6
4	4.3	3.0	7.3
5	9.0	3.0	12.0
6	10.7	3.0	13.7
7	11.9	3.0	14.9
8	12.8	3.0	15.8
9			
10			
11			
12			



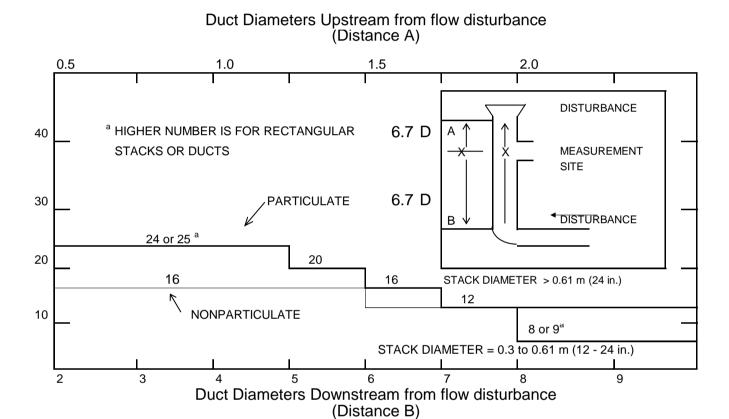
### Figure 4.4 Oxidizer Outlet Sampling Location

### **Sample and Velocity Traverses for Stationary Sources**

Client	Long Island Sterilization	<b>Proj. No.</b> L127-004
Facility		
City, State	Hauppauge, NY	
Test Date		
Test Locat	ion Oxidizer Outlet	
Diameter o	<b>f Stack</b> 17.63	inches

Diameters Upstream of Disturbance (A)	6.7
Diameters Downstream of Disturbance (B)	6.7
Total No. of Traverse Points Required	16
Number of Ports	2
Traverse Points per Port	8
Traverse (Horizontal or Vertical)	Н

### MINIMUM NUMBER OF TRAVERSE POINTS FOR PARTICULATE AND NONPARTICULATE TRAVERSES



## D W Deq = 2LW = \_\_\_\_

17.63 inches

CROSS-SECTIONAL LAYOUT FOR RECTANGULAR STACKS				
I otal	Matrıx			
Traverse Points				
9	3 x 3			
12	4 x 3			
16	4 x 4			
20	5 x 4			
25	5 x 5			

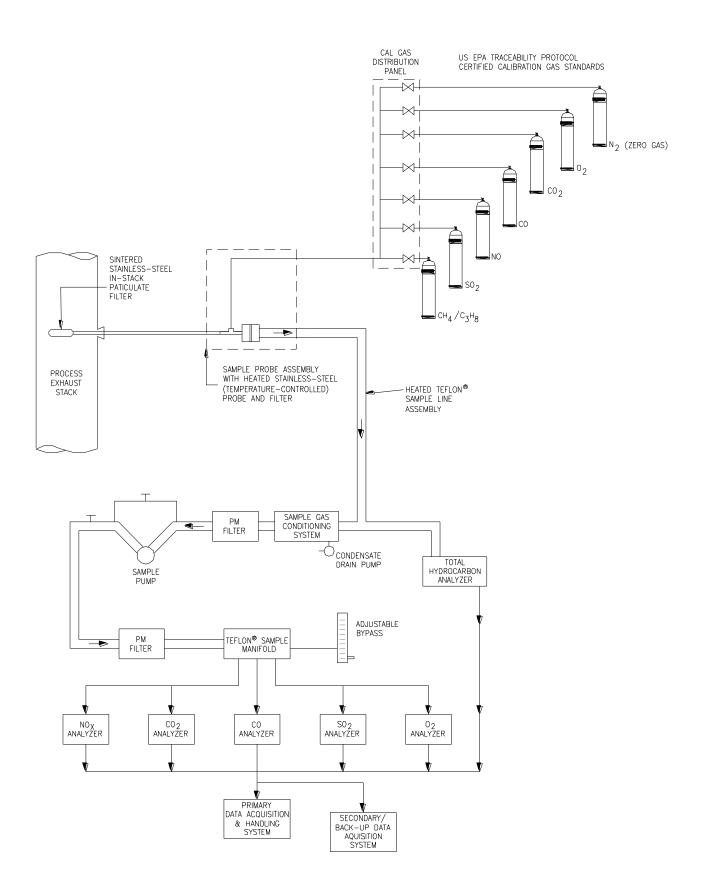
### LOCATION OF TRAVERSE POINTS IN CIRCULAR STACKS

Point Number On A Diameter	(Percent of stack diameter from inside wall to traverse point) Number of Traverse Points on a Diameter 4 6 8 10 12							
1	6.7	4.4	3.2	2.6	2.1			
2	25.0	14.6	10.5	8.2	6.7			
3	75.0	29.6	19.4	14.6	11.8			
4	93.3	70.4	32.3	22.6	17.7			
5		85.4	67.7	34.2	25.0			
6		95.6	80.6	65.8	35.6			
7			89.5	77.4	64.4			
8			96.8	85.4	75.0			
9				91.8	82.3			
10				97.4	88.2			
11					93.3			
12					97.9			

METHOD-1.xls / LGP / rev.2 - 02/97

### TRAVERSE POINT LOCATIONS

No.	Distance from Wall	Port Depth	Total Distance
140.	(inches) (inches)		(inches)
1	0.6	3.0	3.6
2	1.9	3.0	4.9
3	3.4	3.0	6.4
4	5.7	3.0	8.7
5	11.9	3.0	14.9
6	14.2	3.0	17.2
7	15.8	3.0	18.8
8	17.1	3.0	20.1
9			
10			
11			
12			
11	iometer > 24 inche	s minimum 1.0 inch from	otook welle





Long Island Sterilization Hauppauge, New York

Source: ESS Group, Inc.

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ESS Filepath: J:\L127-004 Long Island Ster\Protocol

**CEMS Schematic** 

**Figure** 4.5

# Appendix A Field Data Sheets









PROJECT_	<u>    I                                 </u>	Scrubber Test	PROJECT	NO.	F175	-005
PREPARED BY _	BAD		D	ATE _	7/11	/19
CHECKED BY _			D.	ATE _		
SCALE_			PAGE NO		OF _	l

	: : : : : : : : : : : : : : : : : : : :			
Arı	065. Eb/	BC/KK	clean day 75 F	
0855 20	wh to Nahla B	@ DEC - will	percelal on the south	u terin
	around 1200.	Reschadade o	x testur.	
(215	est Hart 12:	30 at scrubber		
巨-(	Steacles 1	54 act 1234	$b^2 = + c \cdot 31$	
		erd 1275	(1 M L)	
B-2	Sterelzer 2	Start 1241	15 = +0,37	
		erl 1300		
9	Steulzer 1			
12-3	Sterriger 1	start 1616	Vt = 40.30	
		end 1626	(U MIR	
V 1720				
10 (120				
				•



### EPA Method 2 Velocity Traverse and Volumetric Flowrate Determination

Client LIS	Proj. No. 4127-005	Schematic of Stack / Sampling Points
Facility		denotes the death possibility to this
City, State HOUNGE NY		`
Test Date 7/9/19		
Test Location Stubseco	u†	,
Test Run No. P-1	Prelim Traverse	
Stack Dimensions ID. = 9.75	inches. Area (As) = 0.52 f12	lock here
Static Pressure (Pg) = +0.1	φ in. H <sub>2</sub> O	Least check
Barometric Pressure (Pbar) =	29.85 in. Hg	i ;
Stack Gas Molecular Weight (MW) =	25	- 0.20
Stack Gas Moisture Content (Bws x 10	0) = ~27. %	
Pilot No. <u>M2-38 B</u>	Cp = 0.84	
Testen EP/KK		
1615-	1635	

PORT	POINT	DEPTH inches	Delta P inches H,O	T stack ° F	cycl angle ± deg.	Delta P	Delta P x COS Ø
F	(		0.006	91	0		
	2_		0.005		Ī		
	3,		0.006		Ø		
	7		6.011		0		
<b>→</b>	_ <		150,0		<u>0</u> 3		
	Ļ	•	10054		Z		
	7		0.024		í .		
	Ŕ		50.0		· O		
					:		
	(		0.025	91	2 :		
	2		150.0		2		
ا جـــ	3		0.020		1	_	
	۲.		0.00		Ó	· · · · · · · · · · · · · · · · · · ·	
			0.035		1		
	ح		120.0	_	4		
	7		0.030	-	¥		
	ઇ		0.020		5-		
			0.019				
		-					
		, <u>, , , , , , , , , , , , , , , , , , </u>				·	
	AVERA	√Œ √Delta P	0.[35	91			

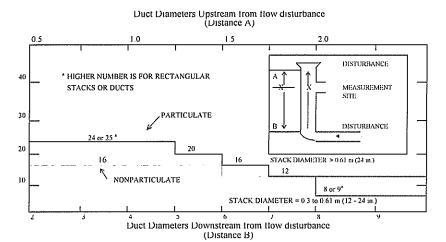
Standard absolute Temperature: Tstd = 528 * R Absolute Gas Temperature: Ts = 460 + Tstk = 55	Standard absolute Pressure: Pstd 29.92 in. Hg
Absolute Stade Gas Pressure: Ps = Poar + (Pg/13.6) = 29.8	in. Hg
Stack Gas Velocity: Vs = (85.49) x Cp x \(\int\)Delta P x COS Ø x	$\frac{1}{\sqrt{15}} = \frac{7.73}{\sqrt{15}}$ fixed
	ACFM
Average Stack Gas Dry Volumetric Flowrate: Qsd = Qa x (1 - Bu	vs) z (Tstd/Ts) z (Ps/Pstd)
= <u>23</u> [ KC1504-2.44]/SF/rev.1 - KH	DSCFM

### EPA Method 1

### Sample and Velocity Traverses for Stationary Sources

Client Proj. No. L127-00	Diameters Upstream of Disturbance (A)	0,6
Facility	Diameters Downstream of Disturbance (B)	2.6
City, State	Total No. of Traverse Points Required	16
Test Date 7919	Number of Ports	2_
Test Location Scrubbly Oct	Traverse Points per Port	8
Diameter of Stack 9.75 inches	Traverse (Horizontal or Vertical)	+-

### MINIMUM NUMBER OF TRAVERSE POINTS FOR PARTICULATE AND NONPARTICULATE TRAVERSES



### 9.75° " D D L L W L L W L+W

CROSS-SECTIONAL LAYOUT FOR RECTANGULAR STACKS					
t otal	Matrix				
Traverse Points					
9	3 x 3				
12	4 x 3				
16	4 x 4				
20	5 x 4				
25	5 x 5				

### LOCATION OF TRAVERSE POINTS IN CIRCULAR STACKS

Point Number On A	(Percent of stack diameter from inside wall to traverse point) Number of Traverse Points on a Diameter 4 6 8 10 12							
Diameter	4	0	<u> </u>	10	12			
1	6.7	4,4	3.2	2.6	2.1			
2	25.0	14.6	10.5	8.2	6.7			
3	75.0	29.6	19.4	14.6	11.8			
4	93.3	70.4	32,3	22.6	17,7			
5	*******	85.4	67.7	34.2	25.0			
6	Ì	95.6	80.6	65.8	35.6			
7			89.5	77.4	64.4			
8			96.8	85.4	75.0			
9				91.8	82.3			
10				97.4	88.2			
11					93.3			
12					97.9			

METHOD-1.xls / LGP / rev.2 - 62/97

### TRAVERSE POINT LOCATIONS

	1 13/1 7 1545	SE FOIRT LOCKITE	מינול
	Distance	Port	Total
No.	from Wall	Depth	Distance
	(inches)	(inches)	(inches)
1	0-5	2.5	3.0
2	1-0		3.5
3	1,9		٨.٧
4	3.1	(`	J.C.
5	رب <i>(</i>	\	9.1
6	7.9		10.4
7	8.7		11.5
8	<i>ې</i> ځې	<b>&gt;</b>	હ
9	•		
10			
11			
12			



PROJECT_	LIS	Sembler Test	PROJE	CT NO.	L127-	-005	
PREPARED BY_				DATE	7/11/1	9	
CHECKED BY _				_ DATE			
SCALE_			_ PAGE NO	(	OF _	(	

		Servites				1/0
212	Time	Scrubber		1227	29.75	36/5
61	1235	+ 0.37 0.37 0.38			No M	-2.
52	1250	0.37 0.37 0.37				
E3	1617	0,37	,	1442	29.75	2.1
	1617 1622 1626	0.35		1555	29.75 4.M=	
+ 1					m = 2.5%	7.
			, 20,000			





## TOTAL HYDROCARBONS DATA SHEET EPA Method 25A

Thermo Environmental 51i	0-600 mm			1234 - 1245	1247 - 1300	1616 - 1626					oncentration	oncentration	
THC Analyzer Data The			Test Times						Acceptance	Criteria	< 5 % of the cylinder concentration	< 5 % of the cylinder concentration	
Manufacturer Model Number	Measurement Range	1		Test 1	Test 2	Test 3			Calibration	Error	0.8	0.8	Predicted Response = (Cylinder Concentration) x (Response Line) Calibration Error =  {Actual Response - Predicted Response} /Cylinder Concentration x 100
									Actual	Response	151.8	2'00€	Predicted Response = (Cylinder Concentration) x (Response Line) rror =  (Actual Response - Predicted Response) /Cylinder Concent
rubber		- Printer and the state of the	Actual	Response	0.0	503.6		Zc)	Predicted	Response	150.6	303.1	Predicted Response ation Error =  (Actual Res
Long Island Sterilization Hauppauge, New York Damas Corporation Wet Scrubber Scrubber Outlet	07/11/19 EP/BC/KK	Calibration Error Test Data	Cylinder	Concentration	0.0	501.6	1.004	Response Line = $(Ha-Za)/(Hc-Zc)$	Cylinder	Concentration	150.0	301.9	Calibr
Client Site Location Source Test Location	Date Testers	THE PRODUCTION OF THE PROPERTY	Calibration	Gas	Zero Gas	High Gas	Response Line		Calibration	Gas	Low Gas	Mid Gas	

	, Milanda (	предоставляний в предоставлений в предос	Calibration Drift Test Data	TOTAL PROPERTY AND A STATE OF THE PROPERTY AND A STATE OF		A VARANTA MARIANTA A VARANTA A	
Calibration	Cylinder	CE Test	Actual	Calibration	Accep	Acceptance	
Gas	Concentration	Response	Response	Drift	Crit	Criteria	
Test Run 1 Zero	0.0	0.0	0.1	0.0	< 3 % of the me	< 3 % of the measurement range	
Test Run 1 High	150.0	151.8	152.7	0.1	< 3 % of the me	< 3 % of the measurement range	
					Test Run 1	123.40	
111111111111111111111111111111111111111					Avg. Conc.		
Test Run 2 Zero	0.0	0.0	0.1	0.0	< 3 % of the me	< 3 % of the measurement range	
Test Run 2 High	150.0	151.8	152.7	0.1	< 3 % of the me	< 3 % of the measurement range	
3743					Test Run 2	97.60	
	***				Avg. Conc.		
Test Run 3 Zero	0.0	0.0	0.1	0.0	< 3 % of the me	< 3 % of the measurement range	
Test Run 3 High	150.0	151.8	153.6	0.3	< 3 % of the me	< 3 % of the measurement range	
	Calibration Drift = ]	Calibration Drift = [(Actual Response - CE Test Response)  *100	st Response)  *100		Test Run 3	101.10	
The state of the s		Measuren	Measurement Range		Avg. Conc.		

		The state of the s	Gas Cylinder Data	The second secon	esse.	CONTROL CONTRO
Calibration	Required	Cylinder	Cylinder	Cylinder	Expiration	Actual
Gas	% of Span	Concentration	Composition	Number	Date	% of Span
Fuel			H,	CC236441		
Combustion Air			Air	CC101713		
Zero Gas	<0.1	0.0	N <sub>2</sub>	EB0116257	10/10/2026	0.0
Low Gas	25-35	150.0	C <sub>3</sub> H <sub>8</sub> / N <sub>2</sub>	CC124954	11/11/23	25.0
Mid Gas	45-55	301.9	C <sub>3</sub> H <sub>8</sub> / N <sub>2</sub>	SG9123960	06/10/25	50.3
High Gas	80-90	501.6	C <sub>3</sub> H <sub>8</sub> / N <sub>2</sub>	CC159282	06/13/25	83.6

### **EPA Method 1-4 Field Data Sheet**Volumetric Flow Rate

Client:	Long Island Sterilization
Facility:	
Site Location:	Hauppauge, New York
Source:	Damas Corporation Wet Scrubber
Test Location:	Scrubber Outlet
Duct Diameter:	9.75 inches
Test Date:	07/11/19
Testers:	EP/BC/KK
Pitot Number:	M2-37b
Pitot Coefficient:	0.84
Test Number:	1
Test Time:	1234 - 1245
Ambient Temperature:	84 F
Barometric Pressure:	29.93 " Hg
Duct Static Pressure:	0.37 <b>" H2O</b>
	Pre / Post
Pitot Leak Checks:	Ok / Ok

l\$	
,	
	•
1	

Traverse

Point

Test

Port

Horiz.

Velocity

Pressure 0.015

Stack Temp. 100.6

Data Summary				
Average Stack Temp.:	100.6 deg. F			
Avg. Sqrt. Delta P:	0.122 " H2O			
Oxygen:	20.9 % dry			
Carbon Dioxide:	0.0 % dry			
Moisture:	2.2 %			
Velocity:	427 fpm			
Volumetric Flow Rate:	221 acfm			
Volumetric Flow Rate:	209 scfm			
Volumetric Flow Rate:	204 dscfm			

### **EPA Method 1-4 Field Data Sheet**Volumetric Flow Rate

Client:	Long Island Sterilization
Facility:	
Site Location:	Hauppauge, New York
Source:	Damas Corporation Wet Scrubber
Test Location:	Scrubber Outlet
Duct Diameter:	9.75 inches
Test Date:	07/11/19
Testers:	EP/BC/KK
Pitot Number:	M2-37b
Pitot Coefficient:	0.84
Test Number:	2
Test Time:	1247 - 1300
Ambient Temperature:	84 F
Barometric Pressure:	29.93 " Hg
Duct Static Pressure:	0.37 " H2O
	Pre / Post
Pitot Leak Checks:	Ok / Ok

	Pre / Post
Pitot Leak Checks:	Ok / Ok
D.L.	
	Summary
Average Stack Temp.:	99.7 deg. F
Avg. Sqrt. Delta P:	0.122 " H2O
Oxygen:	20.9 % dry
Carbon Dioxide:	0.0 % dry
Moisture:	2.2 %
Velocity:	427 fpm
Volumetric Flow Rate:	221 acfm
Volumetric Flow Rate:	209 scfm
Volumetric Flow Rate:	204 dscfm

Test	Traverse	Velocity	Stack
Port	Point	Pressure	Temp.
Horiz.	1	0.015	99.7
		A	
[L			

### **EPA Method 1-4 Field Data Sheet**Volumetric Flow Rate

Client:	Long Island Sterilization
Facility:	
Site Location:	Hauppauge, New York
Source:	Damas Corporation Wet Scrubber
Test Location:	Scrubber Outlet
Duct Diameter:	9.75 inches
Test Date:	07/11/19
Testers:	EP/BC/KK
Pitot Number:	M2-37b
Pitot Coefficient:	0.84
Test Number:	3
Test Time:	1616 - 1626
Ambient Temperature:	84 F
Barometric Pressure:	29.93 " Hg
Duct Static Pressure:	0.36 " H2O
	Pre / Post
Pitot Leak Checks:	Ok / Ok

Pitot Leak Checks: OK / OK		
Data Summary		
Average Stack Temp.:	94.6 deg. F	
Avg. Sqrt. Delta P:	0.122 " H2O	
Oxygen:	20.9 % dry	
Carbon Dioxide:	0.0 % dry	
Moisture:	2.2 %	
Velocity:	425 fpm	
Volumetric Flow Rate:	220 acfm	
Volumetric Flow Rate:	210 scfm	
Volumetric Flow Rate:	205 dscfm	

Test	Traverse	Velocity	Stack
Port	Point	Pressure	Temp.
Horiz.	1	0.015	94.6
<u> </u>			

### Summary of Results Emissions Compliance Testing Damas Corporation Wet Scrubber Long Island Sterilization Hauppauge, New York 07/11/19

Test Number Test Date Test Time		1 07/11/19 1234 - 1245	2 07/11/19 1247 - 1300	3 07/11/19 1616 - 1626	Average	Limit
Scrubber Outlet Flow Rate Data				1		
Duct Temperature	deg. F	100.6	99.7	94.6	98.3	
Oxygen	% dry	20.9	20.9	20.9	20.9	
Carbon Dioxide	% duy	0.0	0.0	0.0	0.0	
Volumetric Flow Rate	acfm	221	221	220	221	
Volumetric Flow Rate	scfm	209	209	210	509	
Scrubber Outlet THC Data	CH.					
Concentration	wwmdd	123.40	97.60	101.10	107.37	
Emission Rate	lb/hr	0.18	0.14	0.15	0.15	

# Appendix B CEMS Data







### Long Island Steerlization

<u>Date</u>	<b>Time</b>	THC PPM (Scrubber Outlet)	
	Calibration E	error Test	
7/11/2019	6:41:29 AM	2.0	
7/11/2019	6:41:59 AM	1.9	
7/11/2019	6:42:29 AM	2.0	
7/11/2019	6:42:59 AM	1.9	
7/11/2019	6:43:29 AM	2.0	
7/11/2019	6:43:59 AM	1.9	
7/11/2019	6:44:29 AM	1.9	
7/11/2019	6:44:59 AM	2.0	
7/11/2019	6:45:29 AM	1.9	
7/11/2019	6:45:59 AM	1.9	
7/11/2019	6:46:29 AM	1.9	
7/11/2019	6:46:59 AM	1.9	
7/11/2019	6:47:29 AM	1.9	
7/11/2019	6:47:59 AM	2.0	
7/11/2019	6:48:29 AM	1.9	
7/11/2019	6:48:59 AM	2.0	
7/11/2019	6:49:29 AM	2.0	
7/11/2019	6:49:59 AM	1.9	
7/11/2019	6:50:29 AM	1.9	
7/11/2019	6:50:59 AM	2.0	
7/11/2019	6:51:29 AM	1.9	
7/11/2019	6:51:59 AM	2.3	
7/11/2019	6:52:29 AM	0.1	
7/11/2019	6:52:59 AM	0.1	
7/11/2019	6:53:29 AM	0.1	
7/11/2019	6:53:59 AM	0.1	
7/11/2019	6:54:29 AM	0.0	
7/11/2019	6:54:59 AM	0.1	
7/11/2019	6:55:29 AM	0.1	
7/11/2019	6:55:59 AM	0.1	
7/11/2019	6:56:29 AM	0.5	
7/11/2019	6:56:59 AM	331.7	
7/11/2019	6:57:29 AM	453.9	
7/11/2019	6:57:59 AM	451.7	
7/11/2019	6:58:29 AM	460.8	
7/11/2019	6:58:59 AM	516.3	
7/11/2019	6:59:29 AM	509.3	
7/11/2019	6:59:59 AM	498.5	
7/11/2019	7:00:29 AM	503.7	
7/11/2019	7:00:59 AM	503.5	
7/11/2019	7:01:29 AM	506.5	
7/11/2019	7:01:59 AM	505.1	
7/11/2019	7:02:29 AM	36.3	
7/11/2019	7:02:59 AM	264.7	
7/11/2019	7:03:29 AM	303.4	

29.93" Hg Ambient cond.

P.1 75

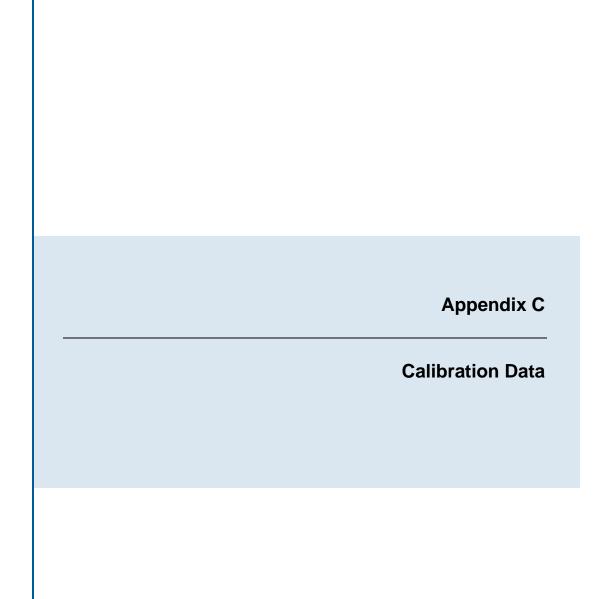
<u>Date</u> 7/11/2019	<u>Time</u> 7:03:59 AM	THC PPM (Scrubber Outlet) 300.1	
7/11/2019	7:04:29 AM	300.6	م ہ
7/11/2019	7:04:59 AM	300.7	p. 2
7/11/2019	7:05:29 AM	302.3	
7/11/2019	7:05:59 AM	300.5	
7/11/2019	7:06:29 AM	205.0	
7/11/2019	7:06:59 AM	152.2	
7/11/2019	7:07:29 AM	152.5	
7/11/2019	7:07:59 AM	152.1	
7/11/2019	7:08:29 AM	151.6	
7/11/2019	7:08:59 AM	151.7	
7/11/2019	7:09:29 AM	151.9	
7/11/2019	7:09:59 AM	152.0	
7/11/2019	7:10:29 AM	152.9	
7/11/2019	7:10:59 AM	153.1	
7/11/2019	7:11:29 AM	115.9	
7/11/2019	7:11:59 AM	51.9	
7/11/2019	7:12:29 AM	51.5	
7/11/2019	7:12:59 AM	51.4	
7/11/2019	7:13:29 AM	51.0	
7/11/2019	7:13:59 AM	48.3	
7/11/2019	7:14:29 AM	94.4	
	Ethylene Oxide Che	ck (300ppm)	
7/11/2019	7:14:59 AM	111.8	
7/11/2019	7:15:29 AM	116.6	
7/11/2019	7:15:59 AM	119.6	
7/11/2019	7:16:29 AM	121.2	
7/11/2019	7:16:59 AM	123.9	124.9
7/11/2019	7:17:29 AM	125.9	RF=2.4
7/11/2019	7:17:59 AM	111.6	
7/11/2019	7:18:29 AM	13.0	
7/11/2019	7:18:59 AM	5.8	
7/11/2019	7:19:29 AM	4.5	
7/11/2019	7:19:59 AM	3.9	
7/11/2019	7:20:29 AM	3.3	
7/11/2019	7:20:59 AM	2.9	
7/11/2019	7:21:29 AM	2.9	
7/11/2019	7:21:59 AM	2.9	

<u>Date</u>	<u>Time</u>	Scrubber Outlet ΔP (" H2O)	Scrubber Outlet °F	THC PPM Scrubber Outlet	
<u>Run 1</u>					
7/11/2019	12:34:00 PM	0.015	100.5	6.7	
7/11/2019	12:34:23 PM	0.015	100.6	6.8	
7/11/2019	12:34:53 PM	0.015	100.8	6.8	
7/11/2019	12:35:23 PM	0.015	101.5	9.7	
7/11/2019	12:35:53 PM	0.015	101.3	40.6	
7/11/2019	12:36:23 PM	0.015	101.2	77.1	
7/11/2019	12:36:53 PM	0.015	100.9	109.0	
7/11/2019	12:37:23 PM	0.015	100.6	133.6	
7/11/2019	12:37:53 PM	0.015	100.7	154.5	
7/11/2019	12:38:23 PM	0.015	100.9	167.6	
7/11/2019	12:38:53 PM	0.015	100.1	177.3	
7/11/2019	12:39:23 PM	0.015	100.3	163.7	
7/11/2019	12:39:53 PM	0.015	101.0	165.6	
7/11/2019	12:40:23 PM	0.015	100.6	168.0	
7/11/2019	12:40:53 PM	0.015	100.7	167.3	
7/11/2019	12:41:23 PM	0.015	100.3	168.5	
7/11/2019	12:41:53 PM	0.015	100.1	166.8	
7/11/2019	12:42:23 PM	0.015	100.8	163.8	
7/11/2019	12:42:53 PM	0.015	100.8	162.0	
7/11/2019	12:43:23 PM	0.015	100.6	158.2	
7/11/2019	12:43:53 PM	0.015	99.8	154.8	
7/11/2019	12:44:23 PM	0.015	99.8	154.9	
7/11/2019	12:44:53 PM	0.015	99.3	155.4	
	Averages:	0.015	100.6	123.4	
	=				
		Run 2			
7/11/2019	12:47:23 PM	0.015	98.9	52.4	
7/11/2019	12:47:53 PM	0.015	99.7	44.3	
7/11/2019	12:48:23 PM	0.015	100.1	63.9	
7/11/2019	12:48:53 PM	0.015	100.1	65.0	
7/11/2019	12:49:23 PM	0.015	100.2	53.9	
7/11/2019	12:49:53 PM	0.015	100.6	55.3	
7/11/2019	12:50:23 PM	0.015	100.6	59.9	
7/11/2019	12:50:53 PM	0.015	100.4	67.2	
7/11/2019	12:51:23 PM	0.015	101.0	77.6	
7/11/2019	12:51:53 PM	0.015	101.1	87.0	
7/11/2019	12:52:23 PM	0.015	100.6	96.1	
7/11/2019	12:52:53 PM	0.015	100.0	103.7	
7/11/2019	12:53:23 PM	0.015	99.6	109.7	
7/11/2019	12:53:53 PM	0.015	100.0	116.4	
7/11/2019	12:54:23 PM	0.015	100.4	121.1	
7/11/2019	12:54:53 PM	0.015	99.7	121.8	
7/11/2019	12:55:23 PM	0.015	99.1	122.8	
7/11/2019	12:55:53 PM	0.015	99.4	126.9 125.3	
7/11/2019	12:56:23 PM	0.015	99.0		
7/11/2019	12:56:53 PM	0.015 0.015	98.9 98.9	124.5 123.7	
7/11/2019	12:57:23 PM 12:57:53 PM	0.015	98.8	123.7	
7/11/2019 7/11/2019	12:57:53 PM 12:58:23 PM	0.015	98.8 98.8	124.3	
1111/2019	12.30.23 FIVI	0.013	70.0	143.1	

P.4

<u>Date</u>	<u>Time</u>	Scrubber Outlet ΔP (" H2O)	Scrubber Outlet *F	THC PPM Scrubber Outlet
7/11/2019	12:58:53 PM	0.015	98.8	124.5
7/11/2019	12:59:23 PM	0.015	99.3	123.7
7/11/2019	12:59:53 PM	0.015	99.0	121.1
	Averages:	0.015	99.7	97.6
	- ;			
		Calibratio	<u>on</u>	
7/11/2019	1:00:23 PM			120.3
7/11/2019	1:00:53 PM			118.7
7/11/2019	1:01:23 PM			102.0
7/11/2019	1:01:53 PM			64.0
7/11/2019	1:02:23 PM			54.7
7/11/2019	1:02:53 PM			73.6
7/11/2019	1:03:23 PM			22.4
7/11/2019	1:03:53 PM			1.2
7/11/2019	1:04:23 PM			0.6
7/11/2019	1:04:53 PM			0.1
7/11/2019	1:05:23 PM			0.0
7/11/2019	1:05:53 PM			0.1
7/11/2019	1:06:23 PM			0.1
7/11/2019	1:06:53 PM		•	87.8
7/11/2019	1:07:23 PM			155.1
7/11/2019	1:07:53 PM			152.9
7/11/2019	1:08:23 PM		[	152.7
7/11/2019	1:08:53 PM			152.7
7/11/2019	1:09:23 PM		•	152.9
7/11/2019	1:09:53 PM			153.0
7/11/2019	1:10:23 PM			125.3
7/11/2019	1:10:53 PM			117.2
		Run 3		
7/11/2019	4:16:00 PM	0.015	94.9	4.9
7/11/2019	4:16:13 PM	0.015	95.2	4.9
7/11/2019	4:16:43 PM	0.015	95.2	4.9
7/11/2019	4:17:13 PM	0.015	95.1	8.8
7/11/2019	4:17:43 PM	0.015	94.8	37.0
7/11/2019	4:18:13 PM	0.015	95.0	66.6
7/11/2019	4:18:43 PM	0.015	94.7	88.5
7/11/2019	4:19:13 PM	0.015	94.9	105.9
7/11/2019	4:19:43 PM	0.015	94.7	121.1
7/11/2019	4:20:13 PM	0.015	94.6	132.4
7/11/2019	4:20:43 PM	0.015	94.1	136.4
7/11/2019	4:21:13 PM	0.015	94.5	141.5
7/11/2019	4:21:43 PM	0.015	94.3	141.9
7/11/2019	4:22:13 PM	0.015	93.8	142.9
7/11/2019	4:22:43 PM	0.015	93.1	142.9
7/11/2019	4:23:13 PM	0.015	93.6	145.8
7/11/2019	4:23:43 PM	0.015	94.4	144.1
7/11/2019	4:24:13 PM	0.015	95.0	142.7
7/11/2019	4:24:43 PM	0.015	95.2	139.4

				4
<u>Date</u>	<u>Time</u>	Scrubber Outlet ΔP (" H2O)	Scrubber Outlet °F	THC PPM Scrubber Outlet
7/11/2019	4:25:13 PM	0.015	94.7	136.9
7/11/2019	4:25:43 PM	0.015	94.3	133.1
	Averages:	0.015	94.6	101.1
		<u>Calibratio</u>	<u>ons</u>	
7/11/2019	4:26:13 PM			133.3
7/11/2019	4:26:43 PM			133.5
7/11/2019	4:27:13 PM			107.2
7/12/2019	4:27:43 PM			66.7
7/13/2019	4:28:13 PM			48.4
7/14/2019	4:28:43 PM			2.0
7/15/2019	4:29:13 PM			0.9
7/16/2019	4:29:43 PM			0.1
7/17/2019	4:30:13 PM			0.1
7/18/2019	4:30:43 PM			0.1
7/19/2019	4:31:13 PM		•	2.4
7/20/2019	4:31:43 PM			109.4
7/21/2019	4:32:13 PM			151.2
7/22/2019	4:32:43 PM			153.6
7/23/2019	4:33:13 PM			153.6
7/24/2019	4:33:43 PM			153.6
7/25/2019	4:34:13 PM			153.6
7/26/2019	4:34:43 PM			153.6
7/27/2019	4:35:13 PM		į.	110,8
,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,	1.55715 1 111			
		ETO Che	<u>ck</u>	
7/28/2019	4:35:43 PM			130.1
7/29/2019	4:36:13 PM			132.0
7/30/2019	4:36:43 PM			131.0
7/31/2019	4:37:13 PM			132.1
8/1/2019	4:37:43 PM			132.5
8/2/2019	4:38:13 PM		133.5	133.3
8/3/2019	4:38:43 PM		RF= 2.2	133.7
8/4/2019	4:39:13 PM		L	74.4
8/5/2019	4:39:43 PM			9.6
8/6/2019	4:40:12 PM			9.6
0/0/2017	7,70,12,1141			<b>,,,</b>











# **CERTIFICATE OF ANALYSIS CEM GRADE NITROGEN**



Customer:

Maine Oxy/ Spec-Air

CGA:

580

Customer PO#:

310024

Cylinder #:

EB0116257

Reference#:

**Certification Date:** 

**Expiration Date:** 

100418SY-Batch A

10/10/2018

10/10/2026

Pressure, psig:

2000

Components	Certified Concentration	Analytical Accuracy
Nitrogen	<u>≥</u> 99.9995%	<del>-</del>
Oxygen	< 0.5 ppm	•
H2O	< 1.0 ppm	-
THC	< 0.1 ppm	-
ÇO2	< 1.0 ppm	~
CO	< 0.5 ppm	÷
NOx	< 0.1 ppm	•
SO2	< 0.1 ppm	*

Serial Number	Last Date Calibrated	Analytical Method
30-0319	10/8/2018	Electrochemical
14469	10/1/2018	Electrolytic
<b>&lt;3560</b> 6	10/10/2018	Flame Ionization Detector
170612	10/10/2018	Thermal Conductivity
3005333138	10/10/2018	Non-Dispersive Infrared
Y09003	10/10/2018	Chemiluminescence
WAID39C8	10/10/2018	Non-Dispersive Infrared
	90-0319 14469 (35606 170612 3005333138 /09003	30-0319     10/8/2018       14469     10/1/2018       K35606     10/10/2018       170612     10/10/2018       30053333138     10/10/2018       709003     10/10/2018

These mixtures were prepared gravimetrically using a high load high sensitivity electronic scale. Prior to filling the scale is verified for accuracy throughout the target mass range against applicable NIST traceable weights. We certify that the weights are calibrated to ASTM E817-97 Echelon 1 tolerances.

This report states accurately the results of the investigation made upon the material submitted to the analytical laboratory. Every effort has been made to determine objectively the information requested. However, in connection with this report, Global Calibration Gases LLC shall have no liability in excess of the established charge for this service. Assayed at Global Calibration Gases LLC, Sarasota, Florida.

250 -	, A.
G	LOBAL
	ALIBRATION
	GASES LLC
-	SAL 9-12 *772-5-2009

and the second s

Produced by:

Global Calibration Gases LLC. 1090 Commerce Blvd N. Sarasota, Florida 34243 USA PGVP Vendor ID.: N22018

Principal Analyst: 10/10/2018 Date:

Principal Reviewer: 1

Date: 10/10/2018



**Airgas Specialty Gases** Airgas USA, LLC 6141 Easton Road Bldg 1 Plumsteadville, PA 18949 Airgas.com

# CERTIFICATE OF ANALYSIS

# **Grade of Product: EPA Protocol**

Part Number: Cylinder Number: E03NI80E15A0138

CC75018

Laboratory:

124 - Plumsteadville - PA

**PGVP Number.** 

A12019

Gas Code:

CO2,O2,BALN

Reference Number: 160-401512444-1

Cylinder Volume:

150.9 CF

Cylinder Pressure:

2015 PSIG

Valve Outlet:

590

Certification Date:

Jun 04, 2019

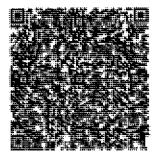
**Expiration Date:** Jun 04, 2027

Certification performed in accordance with "EPA Traceability Protocol for Assay and Certification of Gaseous Calibration Standards (May 2012)" document EPA 600/R-12/531, using the assay procedures listed. Analytical Methodology does not require correction for analytical interference. This cylinder has a total analytical uncertainty as stated below with a confidence level of 95%. There are no significant impurities which affect the use of this calibration mixture. All concentrations are on a volume/volume basis unless otherwise noted.

Do Not Use This Cylinder below 100 psig, i.e. 0.7 megapascals.

			ANALYTICA	L RESULTS		
Compon	ent	Requested Concentration	Actual Concentration	Protocol Method	Total Relative Uncertainty	Assay Dates
CARBON DIOXIDE 10.00 % OXYGEN 10.00 % NITROGEN Balance		10.11 % G1 10.03 % G1		+/- 0.2% NIST Traceal +/- 0.2% NIST Traceal		
Туре	Lot ID	Cylinder No	CALIBRATION Concentration	STANDARD	)S Uncertainty	Expiration Date
NTRM NTRM	060118 120620	K008735 CC367413	23.04 % CARBON DK 22.883 % OXYGEN/N		0.12% 0.22%	Jun 27, 2022 May 14, 2026
Instrume	nt/Make/Mo	del	ANALYTICAL Analytical Pr		T Last Multipoint C	alibration
HORIBA VA5011 T5V6VU9P NDIR CO2 SIEMENS OXYMAT 6 - W5951 - O2		NDIR PARAMAGNETIC		May 10, 2019 May 23, 2019		

Triad Data Available Upon Request



Approved for Release

Page 1 of 160-401512444-1



Airgas Specialty Gases Airgas USA, LLC 600 Union Landing Road Cinnaminson, NJ 08077-0000 Airgus.com

# **CERTIFICATE OF ANALYSIS Grade of Product: EPA Protocol**

Part Number:

E03NI61E15A0287

Cylinder Number:

ALM021415

Laboratory: **PGVP Number:** 

B52018

Gas Code:

124 - Riverton (SAP) - NJ

CO2, O2, BALN

Reference Number: 82-401148361-1

Cylinder Volume:

158.0 CF 2015 PSIG

Cylinder Pressure: Valve Outlet:

590

Certification Date:

Mar 12, 2018

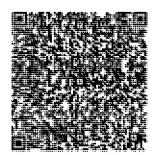
Expiration Date: Mar 12, 2026

Certification performed in accordance with "EPA Traceability Protocol for Assay and Certification of Gaseous Calibration Standards (May 2012)" document EPA 600/R-12/531, using the assay procedures tisted. Analytical Methodology does not require correction for analytical interference. This cylinder has a total analytical uncertainty as stated below with a confidence level of 95%. There are no significant impurities which affect the use of this calibration mixture. All concentrations are on a volume/volume basis unless otherwise noted.

Do Not Use This Cylinder below 100 psig, i.e. 0,7 megapascals.

			ANALYTICA	L RESULTS		
Compon	ent	Requested Concentration	Actual Concentration	Protocol Method	Total Relative Uncertainty	Assay Dates
CARBON DIOXIDE		18.00 %	17.30 %	G1	+/- 0.7% NIST Traceable	
OXYGEN NITROGE	N	21.00 % Balance	20.94 %	G1	+/- 0.5% NIST Traceable	03/12/2018
			CALIBRATION	STANDARD	S	
Type	Lot ID	Cylinder No	Concentration		Uncertainty	Expiration Date
NTRM	12061545	CC354843	19.87 % CARBON D	IOXIDE/NITROGEN	+/- 0,6%	Jan 11, 2024
NTRM	09061420	CC273671	22.53 % OXYGEN/N	ITROGEN	+/- 0.4%	Mar 08, 2019
			ANALYTICAL	EQUIPMENT	1	
instrume	nt/Make/Mod	el	Analytical Princi	ple	Last Multipoint Calib	ration
Horiba VIA	510-CO2-19G	/CXEG	NDIR		Feb 23, 2018	
Horiba MP	A 510-O2-7TW	MJ041	Paramagnetic		Feb 23, 2018	

Triad Data Available Upon Request



Approved for Release

Page 1 of 62-401148361-1

Airgas Specially Gauss Airgas USA, LLC 630 United Drive Durant. MC 27718

# CERTIFICATE OF ANALYSIS

# Grade of Product: EPA Protocol

Part Number: f faring day Ataquagaasi argumani (tangmak); E02NI99E16A2430

Reference Number: 122-401616794-1

Cyllider Velidina.

1,11,1149 #41 9 7 4 44 12414

Latioratory:

124 - Durham (SAP) - NC

Cylinder Pressure:

2015 PSIG

PGVP Number:

B22019

Valve Outlet:

350

Ges Code:

PPN BALN

Certification Date:

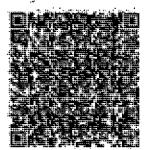
din 11 2019

Expiration Date: Jun 11, 2027

Contification performed in accordance with "EPA Traceability Protocol for Assay and Certification of Geserus Celibration Standards (May 2012)" document EPA 500/7-12/531, using the assay procedures listed. Analytical Methodology does not require convexion for enciption interference. This optimize has a local method before the second field of the continuous control of the continuous control of the continuous control of the c

		130	Not Use This Cylinder be	NOW TUC OSIG, I.O. U.7 MK	одаранска.	
Camponent	neurosie.		ANALYTI	CAL RESULTS	S Tuidi Roldiiya	All rest V
	Concentra		oncentration	<b>Method</b>	Uncertainty	Dates
PROPANE NITROGEN	17.00 PPM Balance	1	8.00 PPM	<b>G</b> 1	+/- 0.6% NIST Trace	able 08/11/2019
Тура	Lot ID	Cylinder No		ON STANDAR	DS Uncertainty	Expiration Date
NTRM	17080914	ND81568	9.800 PPN	PROPANE/AIR	+/- 0.5%	Jul 24, 2023
,			ANALYTICA	L EQUIPME	NT	
Instrument/N	lake/Model		Analytical Prin	ciple	Last Multipoint (	Calibration
Nicolet 6700 Al	HR0801333 C3H6		FTIR		May 23, 2019	

Triad Date Available Upon Request





Airgas Specialty Gases Airgas USA, LLC 630 United Drive Durham, NC 27713 Airgas.com

# CERTIFICATE OF ANALYSIS **Grade of Product: EPA Protocol**

Part Number: Cylinder Number: E02NI99E15A0930

CC410432

124 - Durham (SAP) - NC

Laboratory: **PGVP Number:** Gas Code:

B22019

PPN,BALN

Reference Number: 122-401516793-1

Cylinder Volume:

144.4 CF 2015 PSIG Cylinder Pressure:

Valve Outlet:

350 Certification Date:

Jun 10, 2019

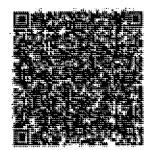
Expiration Date: Jun 10, 2027

Certification performed in accordance with "EPA Traceability Protocol for Assay and Certification of Gaseous Celibration Standards (May 2012)" document EPA 800/R-12/331, using the assay protectures fixed. Analytical Methodology does not require correction for analytical interference. This cylinder has a total enalytical uncertainty as stated below with a confidence level of 98%. There are no algorificant impurities which uffect the use of this calibration mixture. All concentrations are on a volume/volume basis unjust orbited.

Do Not Use This Cylinder below 100 pain, i.e. 0.7 mens

		AN	ALYTICAL RESULT	rs	
Component	Requested Concentra		Protocol tion Method	Total Relative Uncertainty	Assay Dates
PROPANE NITROGEN	30.00 PPM Batence	29.99 PPM	G1	+/- 0.9% NIST Traces	nble 06/10/2019
<b>,</b>		CALIT	RATION STANDA	RDS	
Туре	Lot ID	Cylinder No	Concentration	Uncertainty	Expiration Date
NTRM	00010630	ALM025189	49.8 PPM PROPANE/AIR	+/- 0.6%	Apr 24, 2024
		ANAI	YTICAL EQUIPMI	INT	
instrument/M	lak <del>s/M</del> odel	Analy	tical Principle	Last Multipoint (	Calibration

Triad Data Available Upon Request





Airgas Specialty Gases Airgas USA, LLC 630 United Drive Durham, NC 27713 Alrgau.com

# **CERTIFICATE OF ANALYSIS Grade of Product: EPA Protocol**

Part Number:

E02NI99E15A0931

Cylinder Volume:

Reference Number: 122-401516792-1

Cylinder Number:

CC472820

144,4 CF

Laboratory:

124 - Durham (SAP) - NC

2015 PSIG Cylinder Pressure:

PGVP Number:

B22019

Valve Outlet:

350

Gas Code:

Certification Date:

PPN,BALN

Jun 10, 2019

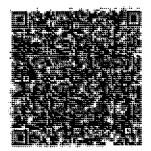
Expiration Date: Jun 10, 2027

Conflication performed in accordance with "EPA Traceability Protocol for Assay and Certification of Gaseous Calibration Standards (May 2012)" document EPA 500/R-12/931, using the seesy procedures listed. Analytical Methodology does not require correction for analytical interference. This cylinder has a total analytical uncertainty as stated below with a confidence level of 95%. There are no significant impurities which affect the use of this calibration mixture. All concentrations are on a volume/volume basis unless otherwise noted.

Do Not Use This Cylinder below 100 palg, i.e. 0.7 mags:

	** P		ANALYTICAL	RESULT	\$	
Component	Requested Concentra		ntration	Protocol Method	Total Relative Uncertainty	Assay Dates
PROPANE NITROGEN	50.00 PPM Balance	50,32 P	PM	G1	+/- 0.8% NIST Traceable	06/10/2019
		CA	LIBRATION	STANDAR	EDS	
Турв	Lot ID	Cylinder No	Concentration	m	Uncertainty	Expiration Date
NTRM	00010630	ALM026189	49.5 PPM PRC	PANE/AIR	+/- 0.6%	Apr 24, 2024
J		Al	NALYTICAL I	QUIPME	NT	
Instrument/M	lake/Model	A	nalytical Principl	<b>)</b>	Last Multipoint Cal	ibration
Nicolet 6700 Al	-IR0801333 C3H8	F	TIR		May 23, 2019	

Triad Data Available Upon Request





Airgas Specialty Gases Airgas USA, LLC 600 Union Landing Road Cinneminson, NJ 08077-0000 Altreas.com

# CERTIFICATE OF ANALYSIS **Grade of Product: EPA Protocol**

Part Number:

E02NI99E15A0581

Cylinder Number:

CC104162

Laboratory: **PGVP Number:** Gas Code:

124 - Riverton (SAP) - NJ

B52017 PPN,BALN Reference Number: 82-401068383-1

Cylinder Volume: Cylinder Pressure:

144.4 CF 2015 PSIG

Valve Outlet:

350

Certification Date:

Dec 27, 2017

Expiration Date: Dec 27, 2025

Certification performed in accordance with "EPA Traceability Protocol for Assay and Certification of Gassous Calibration Standards (May 2012)" document EPA 800/R-12/S31, using the assay procedures listed. Analytical Methodology does not require correction for analytical interference. This cylinder has a total analytical uncertainty as stated below with a confidence level of 95%. There are no significant impurities which affect the use of this calibration mixture. All concentrations are on a volume/volume basis unless otherwise noted.

		Do Not Us	to This Cylinder be	slow 100 paig, i.e. 0.7 m	eg. Sympancais.	
*** *** **** * *** *						and the second of control of the first of the second of th
Component	Requeste Concentr	d Actua		Protocol Method	Total Relative Uncertainty	Assay Dates
PROPANE NITROGEN	85.00 PPM Balance	86.29 F	PM ·	G1	+/- 0.6% NIST Traces	
Туре	Lot ID	CA Cylinder No	LIBRATIC Concent	ON STANDAR		
NTRM	18060319	CC471482		GOODANIEMO	Uncertainty	Expiration Date

99.7 PPM PROPANE/AIR +4 0.5% Nov 16, 2021 ANALYTICAL EQUIPMENT

instrument/Make/Model **Analytical Principle** Last Multipoint Calibration MK\$ 2031 - C3H8 FTIR Dec 27, 2017

Triad Data Available Upon Request



Approved for Release



# **CERTIFICATE OF ANALYSIS**

**Grade of Product: EPA Protocol** 

Airgas, inc.

600 Union Landing Road Chnaminson, NJ 08077 856-829-7878 Fax: 856-829-6576

Part Number:

E02NI99E15A1248

CC124954

ASG - Riverton - NJ

Laboratory: **PGVP Number:** Gas Code:

Cylinder Number:

B52015 PPN,BALN Reference Number:

Cylinder Volume:

Cylinder Pressure:

Valve Outlet: Certification Date:

144.4 CF 2015 PSIG

82-124522206-Airgas.com

350

Nov 11, 2015

**Expiration Date:** 

Nov 11, 2023

Certification performed in accordance with "EPA Traceability Protocol for Assay and Certification of Gaseous Calibration Standards (May 2012)" document EPA 600/R-12/531, using the assay procedures listed. Analytical Methodology does not require correction for analytical interference. This cylinder has a total analytical uncertainty as stated below with a confidence level of 95%. There are no significant impurities which affect the use of this calibration mixture. All concentrations are on a volume/volume basis unless otherwise noted.

Do Not Use This Cyfinder below 100 paig, i.e. 0.7 megapascals

,		ANALYTI	CAL RESULTS	5	
		<del>-,</del>	Protocol Method	Total Relative Uncertainty	Assay Dates
150.0 PPM Balance	150.0	PPM	G1	+/- 0.6% NIST Traces	able 11/11/2015
	C	ALIBRATI	ON STANDAR	DS .	
Lot ID	Cylinder No	Concen	tration	Uncertainty	Expiration Date
14060213	CC428525	249.2 PP	M PROPANE/AIR	+/- 0.5%	Dec 12, 2019
	A	NALYTIC	AL EQUIPMEN	NT	
fake/Model				Last Multipoint C	Calibration
		FTIR		Oct 14, 2015	
	Coricentra 150.0 PPM Balance Lot ID 14060213	Concentration Concentration Concentration Concentration 150.0 PPM 150.0 Balanca C. Lot ID Cylinder No 14060213 CC428525 Affake/Model	Requested Actual Concentration Concentration  150.0 PPM 150.0 PPM Balance  CALIBRATI  Lot ID Cylinder No Concentration  14060213 CC428525 249.2 PP  ANALYTIC Analytical Prince Concentration  Analytical Prince Concentration	Requested Actual Protocol Concentration Concentration Method  150.0 PPM 150.0 PPM G1 Balance  CALIBRATION STANDAR  Lot ID Cylinder No Concentration  14060213 CC428525 249.2 PPM PROPANE/AIR  ANALYTICAL EQUIPME: Analytical Principle	Concentration Concentration Method Uncertainty  150.0 PPM 150.0 PPM G1 +/- 0.6% NIST Traces Balance  CALIBRATION STANDARDS  Lot ID Cylinder No Concentration Uncertainty  14060213 CC428625 249.2 PPM PROPANE/AIR +/- 0.5%  ANALYTICAL EQUIPMENT  Make/Model Analytical Principle Last Multipoint C

Triad Data Available Upon Request



Approved for Release

1.1...

Page 1 of 82-124522206-1



Airgas Specialty Gases Airgas USA, LLC 600 Union Landing Road Cinnaminson, NJ 08077-0000 Airgas.com

# **CERTIFICATE OF ANALYSIS Grade of Product: EPA Protocol**

Part Number:

E02NI99E15A0932

Cylinder Number:

CC159282 124 - Riverton - NJ

Laboratory: **PGVP Number:** Gas Code:

B52017 PPN.BALN

Reference Number: 82-124623100-1 144,4 CF

Cylinder Volume:

Cylinder Pressure:

Valve Outlet: Certification Date:

350

Jun 13, 2017

2015 PSIG

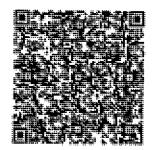
Expiration Date: Jun 13, 2025

Certification performed in accordance with "EPA Traceability Protocol for Assay and Certification of Gaseous Calibration Standards (May 2012)" document EPA 600/R-12/531, using the assay procedures listed. Analytical Methodology does not require correction for analytical interference. This cylinder has a total analytical uncertainty as stated below with a confidence level of 95%. There are no significant impurities which affect the use of this calibration mixture. All concentrations are on a volume/volume basis unless otherwise noted.

Do Not Use This Cylinder below 100 psig, i.e. 0.7 megapascals

		Al	VALYTICAL RESULTS	S	<u> </u>	
Component	Requested Concentrati	Actual on Concent	Protocol ration Method	Total Relative Uncertainty	Assay Dates	
PROPANE NITROGEN	500,0 PPM Balance	501.6 PPN	f G1	+/- 0.6% NIST Traceable	06/13/2017	
Туре	Lot ID	CALI Cylinder No	BRATION STANDAR Concentration	DS Uncertainty	Expiration Date	
NTRMplus	10060506	CC281234	495.3 PPM PROPANE/AIR	+/- 0.5%	Jan 06, 2022	
Instrument/Make/Model			LYTICAL EQUIPMEN cal Principle	MENT Last Multipoint Calibration		
MKS 2031		FTIR		May 17, 2017		

Triad Data Available Upon Request



Approved for Release

# **Airgas**

# CERTIFICATE OF ANALYSIS **Grade of Product: EPA Protocol**

Airgas, inc.

600 Union Landing Road Cinnaminson, NJ 08077

600-626-7676 Fax. 656-829-6576

Part Number: Cylinder Number:

PGVP Number:

Laboratory:

Gas Code:

E02NI99E15A0608

ASG - Riverton - NJ

CC42624

B52014

CH4,BALN

Reference Number:

82-12446737.1-Alrgas.com

Cylinder Volume: Cylinder Pressure: 144.3 CF 2015 PSIG

Valve Outlet:

Certification Date:

350 Dec 11, 2014

**Expiration Date:** 

Dec 11, 2022

Certification performed in accordance with "EPA Traceability Protocol for Assay and Certification of Gaseous Calibration Standards (May 2012)" document EPA 600/R-12/531, using the assay procedures listed. Analytical Methodology does not require correction for analytical interference. This cylinder has a total analytical uncertainty as stated below with a confidence level of 95%. There are no eignificant impurities which affect the use of this calibration mixture. All concentrations are on a volume/volume basis unless otherwise noted.

Do Not Use This Cylinder below 100 psig, i.e. 0.7 megapascals

ANALYTICAL RESULTS							
Component	Requested Concentration	Actual Concentrat	Protocol ion Method	Total Relative Uncertainty	Assay Dates		
METHANE NITROGEN	50.00 PPM Balance	50.96 PPM	G1	+/- 0.8% NIST Traceable	12/11/2014		
CALIBRATION STANDARDS							
Туре	Lot ID	Cylinder No	Concentration	Uncertainty	Expiration Date		
NTRMplus	10061201	CC322737	53.48 PPM METHANE/AIR	+/- 0.7%	Jul 13, 2016		
		ANAL	YTICAL EQUIPME	NT			
Instrument/Ma	ke/Model	Anaiyti	cal Principle	Last Multipoint Calil	Last Multipoint Calibration		
Nicolet 6700 AHR0801933 CH4		FTIR		Dec 11, 2014			

Triad Data Available Upon Request



Approved for Release

Page 1 of 82-124467371-1



# CERTIFICATE OF ANALYSIS **CERTIFIED STANDARD**



Customer:

Maine Oxy/ Spec-Air

CGA:

590

Customer PO#:

331913

Cylinder #:

Eb0127906

Reference#:

061319SY-A

Certification Date:

06/13/2019

**Expiration Date:** 

06/13/2021

Pressure, psig:

2000

Components

Ethylene Oxide Air

Requested Concentration

3ppm Balance **Certified Concentration** 

3.0ppm Balance **Analytical Accuracy** 

± 10%

These mixtures were prepared gravimetrically using a high load high sensitivity electronic scale. Prior to filling the scale is verified for accuracy throughout the target mass range against applicable NIST traceable weights.

This report states accurately the results of the investigation made upon the material submitted to the analytical laboratory. Every effort has been made to determine objectively the information requested. However, in connection with this report, Global Calibration Gases LLC shall have no liability in excess of the established charge for this service.



Produced by:

Global Calibration Gases LLC. 1090 Commerce Blvd N. Sarasota, Florida 34243 PGVP Vendor ID.: N22019

Principal Analyst:

06/13/2019 Date: \_\_\_\_

Principal Reviewer:

Date:



# CERTIFICATE OF ANALYSIS CERTIFIED STANDARD



Customer:

\*PurityPlus\*

Maine Oxy/ Spec-Air

CGA:

590

Customer PO#:

331913

Cylinder #:

EB0127901

Reference#:

061319SY-B

**Certification Date:** 

06/13/2019

**Expiration Date:** 

06/13/2021

Pressure, psig:

2000

Components

Ethylene Oxide Air Requested Concentration

300ppm Balance **Certified Concentration** 

300ppm Balance **Analytical Accuracy** 

± 5%

These mixtures were prepared gravimetrically using a high load high sensitivity electronic scale. Prior to filling the scale is verified for accuracy throughout the target mass range against applicable NIST traceable weights.

This report states accurately the results of the investigation made upon the material submitted to the analytical laboratory. Every effort has been made to determine objectively the information requested. However, in connection with this report, Global Calibration Gases LLC shall have no liability in excess of the established charge for this service.



Produced by:

Global Calibration Gases LLC. 1090 Commerce Blvd N. Sarasota, Florida 34243 PGVP Vendor ID.: N22019

Principal Analyst:

Date: \_\_\_\_\_06/13/2019

Principal Reviewer:

Date: 06/13/201

# SAMPLE PROBE CALIBRATION DATA FORM TYPE "S" PITOT TUBE ASSEMBLY AND NOZZLE

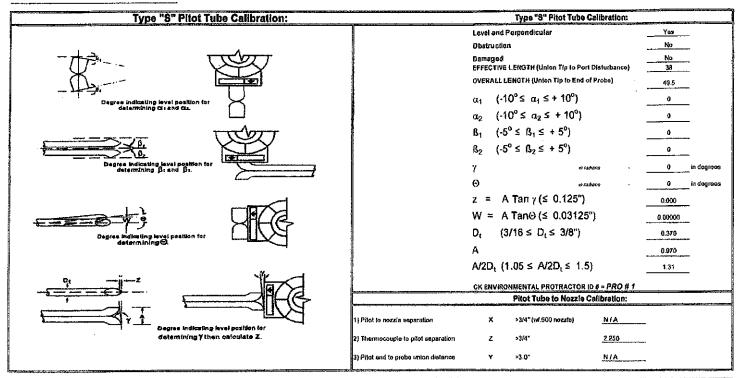
# Thermocouple Calibration

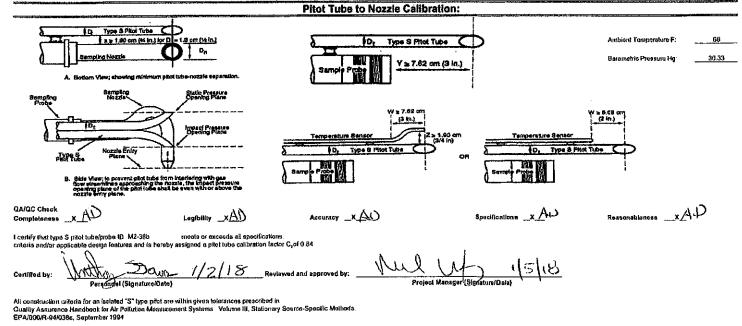
\*CK ASTM mercury-in-glass reference Thermometer: ASTM 2F-99/IP 62F/IBS 593 F 570F/76 MM IMM Serial No. 2196
\*\*CK Termocouple potentiometer ID # = TR - 1

Our sastingsorbing batterings	7.4						The second secon			
	BO	BOILING COOKING CORN OIL			BOILING TAP WATER			STANDARD AMBIENT CONDITIONS		
Themicouple	*Raference	**TC	Temp	"Reference	"TC	Temp	'Reference	"TC	Temp	
ID#	Thermosneter	Temp.	Difference	Thermometer	Temp	Difference	Themometer	Tomp	Difference	
	*K	*K	± 1.5%	•к	ĸ	± 1.5%	K	<u>'K</u>	±1.5%	
		<del></del>	#DIVIO!	373	370.9	-0.6	290.9	292	0.4	
38b		······································	#DIV/0!	373	370.9	-0.6	290.9	292	0.4	
į,	· ·		#DiV/0!	373	370.9	-0.6	290.9	292	0.4	
Averans	N/A	N/A	N/A	373.0	370.90	-0.6	290.90	292.00	0.4	

# DATE: **January 2, 2018**

PROBE ID: M2-38b





K.\Equipment\Probo calibration

CK REVISION 00/06/AR

# Appendix D Process Data







TEST

EO STERILIZER #1 LONG ISLAND STERILIZATION 175 WIRELESS BLVD. HAUPPAUGE, NY 11788 T: 1.631.435.4815

Runi

OPERATOR

DATE 07/11/19 Thu PROG VERSION KORSCP V3Q-1

CYCLE 27

STERILANT EO CHECK VALUE 14543

REK

STACK TEST # / STERILE LOT #

CYL STRAT WT CYL END WI

TIME

580.6 535.0

ETO USED WT 45,6

STERILANT TANK LOT # 190606E000241, TARE WEIGHT: 274.0 LBS

# PROCESS PARAMETERS

CHAMBER TEMP 46 C, BLOWER IS USED

VACUUM A 48.4 KPAA, 6.4 KPA/MIN

NITROGEN DILUTION 2 CYCLES; NITROGEN: 98.0 KPAA, 5.0 KPA/MIN

EVAC: 48.4 KPAA, 6.4 KPA/MIN

GAS A 1 CYCLES; 75.4 KPAA, 2.0 KPA/MIN, EO, LGT 20 C INJ:

90.0 KPAA, 2.0 KPA/MIN, SECOND NITROGEN

GAS DWELL 90.0 KPAA, -1.0 KPA, DWELL 0:10 HH:MM, MAKEUPS: N2

AFTER VACUUM 48.4 KPAA, 6.4 KPA/MIN, HOLD 0:01 HH:MM

GAS WASH A 4 CYCLES; RLS: 94.8 KPAA, 5.0 KPA/MIN, HOLD 0:01 HH:MM, NITR

VAC: 48.4 KPAA, 6.4 KPA/MIN, HOLD 0:01 HH:MM

RELEASE 98.0 KPAA, 7.0 KPA/MIN

PRESS TEMP (DEG C) RH VAP ETO H20

> KPAA AVG 8 GAS MG/L MG/L ALARMS & MESSAGES

ACTION TAKEN

11:05 EXISTING HIDI OVERRIDES:

BlwrOK to MAN ON ExhVlv to MAN OFF Blower to MAN ON

# VACUUM A PHASE

11:05	99.4	46.3	33.3 -200 -39.9	
11:06	95.5	45.8	33.3 -200 -39.9	
11:07	90.7	44.7	33.3 -200 -39.9	
11:07	90.3	44.6	33.3 -200 -39.9	SLOW EVACUATION
11:08	86.1	43.9	33.3 -200 -39.9	
11:09	81.6	43.5	33.3 -200 -39.9	
11:10	77.1	43.2	33.3 -200 -39.9	
11:11	72.9	43.0	33.3 -200 -39.9	
11:12	68.9	42.9	33.3 -200 -39.9	
11:13	65.0	42.7	33.3 -200 -39.9	
11:14	61.2	42.7	33.3 -200 -39.9	
11:15	57.5	42.6	33.4 -200 -39.9	
11:16	54.0	42.5	33.4 -200 -39.9	
11:17	50.7	42.5	33.4 -200 -39.9	

		CP V3Q-1 0 STACK TEST 2	7/11/19 Thu	11:17	CYCLE 27 CHECK VALUE 14543
TIME	PRESS KPAA	TEMP (DEG C) AVG			ALARMS & MESSAGES ACTION TAKEN
11:17	48.4	42.4	33.4 -200	-39.9	
MAX: MIN:	99.4 48.4	46.3 42.4	33.4 -200 33.3 0		PHASE 0:12 PHASE ELAPSED 0:12 CYCLE 0:12
			NITROGEN DI	LUTION	PHASE
11:17 11:18 11:19 11:20 11:21 11:22 11:23 11:24 11:25 11:25 11:29 11:29 11:30 11:31 11:32 11:33 11:34 11:35 11:39 11:39 11:39 11:39 11:40 11:41 11:42 11:43 11:45 11:45 11:45 11:45 11:50 11:51 11:51 11:52 11:53 11:54	53.5 58.5 63.5 68.6 73.6 78.6 83.5 93.6 93.6 98.0 93.6 88.3 84.0 79.6 75.2 71.0	42.4 43.57 445.7 48.6 48.6 48.6 48.7 48.6 48.7 48.6 48.7 48.6 48.7 48.3 48.3 48.4 48.5 48.7 48.7 48.7 48.7 48.7 48.7 48.7 48.7	33.4 -200 33.4 -200	999999999999999999999999999999999999999	
11:55 11:56 11:57	71.0 67.0 63.2	43.0 42.9 42.7	33.5 -200 33.5 -200 33.5 -200	-39.9	

DDI ANTAF STERILE I		CP V3Q-1 0 STACK TEST 2	7/11/19 Thu	11:58	CYCLE	27	CHECK VALUE	1.4543
TIME	PRESS KPAA	TEMP (DEG C) AVG	RH VAP ETO % GAS MG/		ALARMS & ME	SSAGES	ACTION TA	KEN
11:58 11:59 12:00 12:01 12:01	59.4 55.8 52.4 49.0 48.4	42.6 42.5 42.4 42.3 42.3	33.5 -20 33.5 -20 33.5 -20 33.5 -20 33.5 -20	0 -39.9 0 -39.9 0 -39.9				
MAX: MIN:	98.0 48.3	48.8 42.3	33.5 -20 33.4		PHASE	0:43	PHASE ELAPSE CYCL	
			GAS A (EO)	PHASE	Add ETO			
12:22	87.6 89.6	42.3 43.0 44.8 46.0 46.6 46.9 46.9 46.9 46.8 46.8 46.8 46.8 47.0 47.0 47.0 47.1 47.1	33.6 -200	0 -39.9 0 -39.9				
MAX: MIN:		47.1 42.3			PHASE	0:20	PHASE ELAPSEI CYCLI	
	ESTIMA:	TED STERILANT	USED THIS PH	ASE:	45.9, CYCL	E TOTAL:	45.9	
			GAS DWELL	(EO) PHA	SE			
12:23 12:24 12:25 12:26 12:27 12:27	90.2 90.2 90.2 90.2 90.2 90.2	47.1 46.8 46.5 46.4 46.3 46.2 46.2	33.6 -200 33.6 -200 33.6 -200 33.6 -200 33.6 -200 33.6 -200	0 -39.9 0 -39.9 0 -39.9 0 -39.9 0 -39.9 0 -39.9			OPERATOR (	CYCLE STOF

	DDI ANTAE STERILE I		CP V3Q-1 0 STACK TEST 2	7/11/19 T	hu	12:29	CYCLE	27	CHECK VALUE 1	4543
	TIME	PRESS KPAA	TEMP (DEG C) AVG	RH VAP % GAS			ALARMS & MES	SAGES	ACTION TAK	EN
	12:29 12:30 12:30 12:31 12:32 12:32	90.2 90.3 90.3 90.3 90.3	46.2 46.2 46.2 46.2 46.2	33.6 33.6 33.6 33.6	-200 -200 -200 -200	-39.9 -39.9			CYCLE CONT	INUED
	MAX: MIN:	90.3 90.1	47.1 46.2				PHASE	0:10	PHASE ELAPSED CYCLE	
				AFTER V	ACUU	M PHASE				
	12:32 12:33 12:34 12:35 12:36 12:37 12:38 12:39 12:40 12:41 12:42	90.3 86.7 81.6 77.0 72.6 68.5 64.7 61.0 57.4 54.0 50.7	46.2 45.0 44.3 43.9 43.7 43.6 43.5 43.4 43.3	33.6 33.6 33.6 33.6 33.6 33.6	-200 -200 -200 -200 -200 -200 -200 -200	-39.9 -39.9 -39.9 -39.9 -39.9 -39.9 -39.9 -39.9	STA RT	Evac-	-	
<del>-&gt;</del>	12:43 12:43 12:44 12:44	48.4 48.4 48.4 48.4	43.2	33.7 · 33.7 · 33.7 ·	-200 -200 -200	-39.9 -39.9	EVACUATION PI		CUUM HOLD====	
	MAX: MIN:	90.3 48.4	46.2 43.2	33.7 - 33.6		-39.9 0.1	PHASE	0:11	PHASE ELAPSED CYCLE	
				GAS WASI	H A	PHASE				
	12:44 12:45 12:46 12:47 12:48 12:49	48.4 53.7 58.7 63.7 68.7 73.7	43.5 45.1 46.7 47.5 48.1 48.2	33.7 - 33.7 - 33.7 - 33.7 - 33.7 - 33.7 -	-200 -200 -200 -200	-39.9 -39.9 -39.9 -39.9	======================================	ELEASE	1 ==========	
	12:50 12:51 12:52 12:52 12:53 12:54 12:55 12:56 12:57 12:58	78.7 83.7 88.7 93.2 93.4 92.9 92.9 92.9 92.9	48.4 48.4 48.4 48.4 48.0 47.1 46.7 46.5 46.3	33.6 - 33.6 - 33.6 - 33.6 - 33.6 - 33.6 - 33.6 -	-200 -200 -200 -200 -200 -200 -200 -200	-39.9 -39.9 -39.9 -39.9 -39.9 -39.9 -39.9 -39.9			OPERATOR C	
	12:59	92.9	46.4	33.7 -	-200	-39.9			CYCLE CONT	INUED

DDI ANTARES KORSCP V3Q-1 07/11/19 Thu 12:59 CYCLE 27 CHECK VALUE 14543 STERILE LOT # STACK TEST 2

TIME	PRESS KPAA	TEMP (DEG C) AVG	RH VAP ETO H2O % GAS MG/L MG/L	ALARMS & MESSAGES ACTION TAKEN
12:59	92.9	46.4	33.7 -200 -39.9	
12:59	94.8	46.4	33.7 -200 -39.9	======= RELEASE HOLD 1 =======
13:00	94.8	46.8	33.7 -200 -39.9	Marie and April Pric Indiana at the
13:00	94.8	46.8	33.7 -200 -39.9	======================================
13:01	90.5	46.5	33.7 -200 -39.9	
13:02	85.6	45.2	33.7 -200 -39.9	CIT ALL THIS CITS HT AST
13:02	85.2	45.1	33.7 -200 -39.9	SLOW EVACUATION
13:03	81.1	44.4	33.7 -200 -39.9	
13:04 13:05	76.7 72.6	44.0 43.7	33.6 -200 -39.9 33.6 -200 -39.9	
13:05	68.7	43.6	33.6 -200 -39.9	
13:07	64.8	43.4	33.6 -200 -39.9	
13:08	61.0	43.3	33.6 -200 -39.9	
13:09	57.4	43.2	33.6 -200 -39.9	
13:10	54.0	43.1	33.6 -200 -39.9	
13:11	50.7	43.1	33.6 -200 -39.9	
13:12	48.4	$\frac{1}{43.0}$	33.6 -200 -39.9	EVACUATION PRESSURE
13:12	48.4	43.0	33.6 -200 -39.9	======================================
13:13	48.5	43.3	33.6 -200 -39.9	
13:13	48.4	43.6	33.6 -200 -39.9	======================================
13:14	53.7	45.2	33.6 -200 -39.9	
13:15	58.6	46.9	33.6 -200 -39.9	
13:16	63.7	47.8	33.6 -200 -39.9	
13:17	68.6	48.3	33.6 -200 -39.9	
13:18	73.7	48.4	33.6 -200 -39.9	
13:19	78.7	48.6	33.6 -200 -39.9	
13:20	83.7	48.6	33.6 -200 -39.9	
13:21	88.7	48.6	33.6 -200 -39.9	
13:22	93.6	48.6	33.6 -200 -39.9	
13:22	94.8	48.7	33.6 -200 -39.9	====== RELEASE HOLD 2 =======
13:23	94.6	48.1	33.6 -200 -39.9	
13:23	94.6	48.1	33.6 -200 -39.9	====== EVACUATION 2 =======
13:24 13:25	90.2 85.2	47.0	33.6 -200 -39.9 33.6 -200 -39.9	
13:25	84.8	45.3 45.2	33.6 -200 -39.9	SLOW EVACUATION
13:26	80.6	44.4	33.6 -200 -39.9	DIOM EAUCOUTION
13:27	76.3	43.9	33.6 -200 -39.9	
13:28	72.1	43.6	33.6 -200 -39.9	
13:29	68.2	43.4	33.6 -200 -39.9	
13:30	64.3	$\frac{1}{43.3}$	33.6 -200 -39.9	
13:31	60.5	43.2	33.6 -200 -39.9	
13:32	56.8	43.1	33.6 -200 -39.9	
13:33	53.5	43.0	33.6 -200 -39.9	
13:34	50.1	43.0	33.6 -200 -39.9	
13:35	48.4	43.0	33.6 -200 -39.9	EVACUATION PRESSURE
13:35	48.4	43.0	33.6 -200 -39.9	======================================
13:36	48.5	43.3	33.6 -200 -39.9	
13:36	48.4	43.5	33.6 -200 -39.9	======= RELEASE 3 ===========
13:37	53.6	45.1	33.6 -200 -39.9	
13:38	58.6	46.7	33.6 -200 -39.9	
13:39	63.6	47.7	33.6 -200 -39.9	
13:40	68.6	48.3	33.6 -200 -39.9	

DDI ANTARES KORSCP V3Q-1 07/11/19 Thu 13:41 CYCLE 27 CHECK VALUE 14543 STERILE LOT # STACK TEST 2

TIME	PRESS KPAA	TEMP (DEG C) AVG	RH VAP ETO % GAS MG/L	H2O MG/L	ALARMS & MESSAGES	ACTION TAKEN
13:41	73.7	48.6	33.6 -200	_39.9		
13:42	78.7	48.7	33.6 -200			
13:43	83.7	48.7	33.6 -200			
13:44	88.7	48.7	33.6 -200			
13:45	93.6	48.8	33.6 -200			
13:45	94.8	48.8	33.6 -200		======================================	
13:46	94.6	48.2	33.6 -200			
13:46	94.6	48.2	33.6 -200		======== EVACUATION	3
13:47	90.1	47.1	33.6 -200		tomas A to the south of the total of the tot	
13:48	85.1	45.3	33.6 -200			
13:48	84.7	45.2	33.6 -200	-39.9	SLOW EVACUATION	
13:49	80.5	44.3	33.6 -200	-39.9		
13:50	76.1	43.8	33.6 -200	-39.9		
13:51	71.9	43.6	33.6 -200	-39.9		
13:52	67.9	43.4	33.6 -200	-39.9		
13:53	64.1	43.3	33.6 -200	-39.9		
13:54	60.3	43.2	33.6 -200	-39.9		
13:55	56.6	43.0	33.6 -200	-39.9		
13:56	53.2	42.9	33.6 -200			
13:57	49.8	42.9	33.6 -200			
13:58	48.4	42.9	33.6 - 200		EVACUATION PRESSURE	
13:58	48.4	42.9	33.6 -200		======= VACUUM HOLD	3
13:59	48.5	43.2	33.6 -200			
13:59	48.4	43.5	33.6 -200		======================================	
14:00	53.6	45.0	33.6 -200			
14:01	58.6	46.7	33.6 -200			
14:02	63.7	47.8	33.6 -200			
14:03 14:04	68.7 73.6	48.4	33.6 -200			
14:0 <del>4</del> 14:05		48.7	33.6 -200			
14:05	78.7 83.7	48.8 48.9	33.6 -200			
14:07	88.6	40.9 48.8	33.6 -200 33.6 -200		•	
14:08	93.6	48.8	33.6 -200			
14:08	94.8	48.8	33.6 -200		======= RELEASE HOLD	4
14:09	94.5	48.2	33.6 -200			
14:09	94.5	48.2	33.6 -200		====== EVACUATION	4
14:10	90.1	47.0	33.6 -200		HVIIOOILLOW	
14:11	85.1	45.2	33.6 -200			
14:11	84.7	45.1	33.6 -200		SLOW EVACUATION	
14:12	80.5	44.2	33.6 -200			
14:13	76.1	43.7	33.6 -200			
14:14	71.9	43.4	33.6 -200	-39.9		
14:15	67.9	43.2	33.6 -200	-39.9		
14:16	64.0	43.1	33.6 -200			
14:17	60.1	43.0	33.6 -200 ·			
14:18	56.5	42.9	33.6 -200			
14:19	53.1	42.8	33.6 -200 ·			
14:20	49.7	42.7	33.6 -200			
14:21	48.4	42.7	33.6 -200			
14:21	48.4	42.7			======== VACUUM HOLD	Amount of the second se
14:22	48.5	43.0	33.6 -200	-39.9		

DDI ANTAF STERILE I		CP V3Q-1 C STACK TEST 2	7/11/19 Thu	14:22	CYCLE	27	CHECK VALUE	14543	
TIME	PRESS KPAA	TEMP (DEG C) AVG		H2O MG/L	ALARMS & MES	SAGES	ACTION TA	AKEN	
14:22	48.4	43.3	33.6 -200	-39.9					
MAX: MIN:	94.8 48.4	48.9 42.7	33.7 -200 33.6 0		PHASE	1:32	PHASE ELAPSE CYCI		
	RELEASE PHASE								
14:22 14:23 14:24 14:24 14:25 14:26 14:27 14:28 14:30 14:31 14:32 14:33 14:34 14:35 14:35 14:37 14:37 14:37 14:36 14:37	48.3 48.3 51.6 54.7 55.0 57.8 60.7 63.5 66.2 68.8 71.3 73.6 75.9 78.0 80.1 82.0 83.8 85.5 87.1 88.6 94.7 95.4 96.6 96.6	43.3 44.5 46.0 46.2 47.5 47.5 47.5 47.5 47.3 47.3 47.1 47.1 47.0 47.0 46.9 46.9	33.6 -200 33.6 -200	-39.9 -39.9 -39.9 -39.9 -39.9 -39.9 -39.9 -39.9 -39.9 -39.9 -39.9 -39.9 -39.9 -39.9	LOOSEN DOOR I				
14:44 14:45 14:46	97.2 97.7 98.0	46.9 46.8 46.8	33.6 -200 33.6 -200 33.6 -200	-39.9					
MAX: MIN:	98.0 48.3	47.5 43.3	33.6 -200 33.6 0	-39.9	PHASE	0:23	PHASE ELAPSE CYCL		
	CYCLE COMPLETE PHASE								
14:46					TOTAL CYCLE	3:31	CYCLE ELAPSE	D 3:41	

SIGNATURES: OPERATOR

SUPERVISOR

TrST 2

EO STERILIZER #2 LONG ISLAND STERILIZATION 175 WIRELESS BLVD. HAUPPAUGE, NY 11788 T: 1.631.435.4815

Run Z

DATE 07/11/19 Thu PROG VERSION KORSCP V30-1

STACK TEST 1

STERILANT EO

CHECK VALUE 14543

OPERATOR

REK

CYL START WI CYL END WI

ETO USED WT

TIME

STERILE LOT #

548-4

STERILANT TANK LOT # 190606E006303, TARE WEIGHT: 292.0 LBS

# PROCESS PARAMETERS

CYCLE 27

CHAMBER TEMP 46 C, BLOWER IS USED

VACUUM A 48.4 KPAA, 6.4 KPA/MIN

NITROGEN DILUTION 2 CYCLES; NITROGEN: 98.0 KPAA, 5.0 KPA/MIN

EVAC: 48.4 KPAA, 6.4 KPA/MIN

75.4 KPAA, 2.0 KPA/MIN, EO, LGT 20 C GAS A 1 CYCLES; INJ:

90.0 KPAA, 2.0 KPA/MIN, SECOND NITROGEN

GAS DWELL 90.0 KPAA, -1.0 KPA, DWELL 0:10 HH:MM, MAKEUPS: N2

AFTER VACUUM 48.4 KPAA, 6.4 KPA/MIN, HOLD 0:01 HH:MM

GAS WASH A 4 CYCLES; RLS: 94.8 KPAA, 5.0 KPA/MIN, HOLD 0:01 HH:MM, NITR

VAC: 48.4 KPAA, 6.4 KPA/MIN, HOLD 0:01 HH:MM

RELEASE 98.0 KPAA, 7.0 KPA/MIN

PRESS TEMP (DEG C) RH VAP ETO H20

> % GAS MG/L MG/L AVG ALARMS & MESSAGES ACTION TAKEN **KPAA**

11:11 EXISTING HIDI OVERRIDES:

BlwrOK to MAN ON ExhVlv to MAN OFF Blower to MAN ON

# VACUUM A PHASE

11:11	99.9	46.3	53.6 -200 -39.9	
11:12	96.9	46.1	53.6 -200 -39.9	
11:13	92.9	45.1	53.6 -200 -39.9	
11:13	92.6	45.1	53.6 -200 -39.9 SLOW EVACUATION	
11:14	89.1	44.5	53.6 -200 -39.9	
11:15	85.2	44.0	53.5 -200 -39.9	
11:16	81.3	43.7	53.5 -200 -39.9	
11:17	77.4	43.5	53.5 -200 -39.9	
11:18	73.8	43.3	53.5 -200 -39.9	
11:19	70.2	43.2	53.5 -200 -39.9	
11:20	66.9	43.2	53.4 -200 -39.9	
11:21	63.7	43.1	53.4 -200 -39.9	
11:22	60.5	43.1	53.3 -200 -39.9	
11:23	57.5	43.0	53.3 -200 -39.9	
11:24	54.6	43.0	53.3 -200 -39.9	

DDI ANTARES KORSCP V3Q-1 07/11/19 Thu 11:25 CYCLE 27 CHECK VALUE 14543 STERILE LOT # STACK TEST 1

TIME	PRESS KPAA	TEMP (DEG C) AVG	RH VAP ETO H2O % GAS MG/L MG/L	ALARMS & MESSAGES ACTION TAKEN
11:25	51.7	43.1	53.2 -200 -39.9	
11:26	49.0	43.0	53.2 -200 -39.9	
11:26	48.4	43.0	53.2 -200 -39.9	
MAX:	99.9	46.3	53.6 -200 -39.9	PHASE 0:15 PHASE ELAPSED 0:15
MIN:	48.4	43.0	53.2 0 0.1	CYCLE 0:15
			NITROGEN DILUTION	PHASE
11:26	48.4	43.0	53.2 -200 -39.9	======= NITROGEN 1 =========
11:27	54.2	44.0	53.2 -200 -39.9	
11:28	59.2	46.2	53.2 -200 -39.9	
11:29	64.1	47.4	53.1 -200 -39.9	
11:30	69.2	48.0	53.0 -200 -39.9	
11:31	74.2	48.3	53.1 -200 -39.9	
11:32	79.1	48.4	53.0 -200 -39.9	
11:33	84.2	48.5	53.0 -200 -39.9	
11:34	89.2	48.5	52.9 -200 -39.9	
11:35	94.2	48.5	52.9 -200 -39.9	TELACHIAMITONI 1
11:36 11:37	98.0 94.9	48.4 48.1	52.9 -200 -39.9 52.9 -200 -39.9	====== EVACUATION 1 ========
11:37	90.8	46.3	52.8 -200 -39.9	
11:38	90.5	46.2	52.8 -200 -39.9	SLOW EVACUATION
11:39	86.8	45.1	52.7 -200 -39.9	STOM EAUCOVITOR
11:40	83.0	44.2	52.7 -200 -39.9	
11:41	79.1	43.7	52.5 -200 -39.9	
11:42	75.3	43.5	52.6 -200 -39.9	
11:43	71.7	43.2	52.5 -200 -39.9	
11:44	68.3	43.1	52.5 -200 -39.9	
11:45	65.0	43.1	52.5 -200 -39.9	
11:46	61.9	43.0	52.5 -200 -39.9	
11:47	58.8	43.0	52.4 -200 -39.9	
11:48	55.8	43.0	52.2 -200 -39.9	
11:49	52.9	42.9	52.2 -200 -39.9	
11:50	50.1	43.0	52.3 -200 -39.9	
11:50	48.4	42.9	52.2 -200 -39.9	======= NITROGEN 2 ===========
11:51	54.2	44.0	52.2 -200 -39.9	
11:52	59.2	46.2	52.2 -200 -39.9	
11:53 11:54	64.2 69.2	47.4 48.0	52.3 -200 -39.9 52.4 -200 -39.9	
11:54	74.2	48.3	52.5 -200 -39.9	
11:56	79.1	48.5	52.6 -200 -39.9	
11:57	84.2	48.5	52.7 -200 -39.9	
11:58	89.2	48.4	52.9 -200 -39.9	
11:59	94.2	48.4	53.1 -200 -39.9	
12:00	98.0	48.4	53.2 -200 -39.9	======= EVACUATION 2 ========
12:01	94.9	48.0	53.2 -200 -39.9	
12:02	90.7	46.3	53.3 -200 -39.9	
12:02	90.4	46.1	53.3 -200 -39.9	SLOW EVACUATION
12:03	86.8	45.0	53.4 -200 -39.9	
12:04	82.9	44.2	53.3 -200 -39.9	
12:04	82.4	44.1	53.3 -200 -39.9	OPERATOR CYCLE STOP
12:04	82.3	44.0	53.3 -200 -39.9	CYCLE CONTINUED

DDI ANTARES KORSCP V3Q-1 07/11/19 Thu 12:04 CYCLE 27 CHECK VALUE 14543

STERILE LOT	T.	STACK	TEST	1
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TIME	PRESS KPAA	TEMP (DEG C) AVG	RH VAP ETO H2O % GAS MG/L MG/L ALARMS & MESSAGES ACTION TAKEN
	=		
12:05	79.0	43.6	53.3 -200 -39.9
12:06	75.2	43.3	53.3 -200 -39.9 53.4 -200 -39.9
12:07	71.6	43.0	
12:08	68.1	43.0	53.4 -200 -39.9
12:09	64.9	42.9	53.4 -200 -39.9
12:10	61.7	42.9	53.5 -200 -39.9
12:11	58.7	42.9	53.5 -200 -39.9
12:12	55.7	42.9	53.6 -200 -39.9
12:13	52.8	42.8	53.5 -200 -39.9
12:14	50.0	42.8	53.5 -200 -39.9
12:15	48.4	42.8	53.5 -200 -39.9
MAX:	98.0	48.5	53.6 -200 -39.9 PHASE 0:48 PHASE ELAPSED 0:48
MIN:	48.4	42.8	52.2 0 0.1 CYCLE 1:03
			GAS A (EO) PHASE AR ETO
<b>→12:15</b>	48.4	42.8	53.5 -200 -39.9 ======== STERILANT 1 ==========
12:15	50.9	43.3	53.5 -200 -39.9 STERTEANT 1
12:17	52.7	44.7	53.3 -200 -39.9
12:18	54.8	45.5	53.0 -200 -39.9
12:19	56.8	46.0	52.8 -200 -39.9
12:20	58.7	46.3	52.5 -200 -39.9
12:21	60.7	46.4	52.3 -200 -39.9
12:22	62.8	46.5	52.0 -200 -39.9
12:23	64.8	46.5	51.9 -200 -39.9
12:23	66.7	46.5	51.6 -200 -39.9
12:25	68.8	46.5	51.4 -200 -39.9
12:26	70.7	46.5	51.4 -200 -39.9
12:20	72.7	46.5	51.2 -200 -39.9
12:28	74.7	46.5	51.2 -200 -39.9
12.28 ≯12:28	75.4	46.5	51.1 -200 -39.9 ======= SECOND NITROGEN 1 =======
12:29	$\frac{73.4}{78.0}$	46.8	50.8 -200 -39.9
12:29	80.1	46.8	50.8 -200 -39.9
12:31	82.1	46.8	50.8 -200 -39.9
12:32	84.1	46.8	50.7 -200 -39.9
12:33	86.1	46.8	50.6 -200 -39.9
12:34	88.1	46.8	50.6 -200 -39.9
12:34	90.0	46.8	50.6 -200 -39.9
MAX:	90.0	46.8	53.5 -200 -39.9 PHASE 0:19 PHASE ELAPSED 0:19
MIN:	48.4	42.8	50.6 0 0.1 CYCLE 1:23
	ESTIMAT	ED STERILANT	USED THIS PHASE: 46.1, CYCLE TOTAL: 46.1
			GAS DWELL (EO) PHASE
12:34	90.1	46.8	50.6 -200 -39.9
12:35	90.0	46.8	50.6 -200 -39.9
12:36	90.0	46.4	50.4 -200 -39.9

DDI ANTARES KORSCP V3Q-1 07/11/19 Thu 12:37 CYCLE 27 CHECK VALUE 14543 STERILE LOT # STACK TEST 1

TIME	PRESS KPAA	TEMP (DEG C) AVG		P ETO S MG/L	H2O MG/L	ALARMS & MESSAGES	ACTION TAKEN
2 1.1/22	TET THY	1100		3 1,20, 23	1:0/13	THE HELD CE PHOTOLOGIC	TAGE LOW EXECUTE
12:37	90.0	46.2	50.	1 -200	-39.9		
12:38	90.0	46.1	49.	3 -200	-39.9		
12:39	90.0	46.1	49.	5 -200	-39.9		
12:40	90.1	46.0	49.	3 -200	-39.9		
12:41	90.1	46.0	49.	2 - 200	-39.9		
12:42	90.1	45.9	49.0	200	-39.9		
12:43	90.1	45.9			-39.9		
12:44	90.1	45.9			-39.9		
12:44	90.1	45.9	48.3	3 -200	-39.9		
MAX:	90.1	46.8	50 (	5 200	-39.9	PHASE 0:10	PHASE ELAPSED 0:10
MIN:	90.0	45.9	48.8			THESE O.TO	CYCLE 1:33
* PI 11/1	30.0	43.9	70.0	, ,	0.1		CICED 1.33
			AFTER	VACTUR	M PHASE		
			IN REAL	411000I	· · · · · · · · · · · · · · · · · · ·	EVAC - Z	
×12:44	90.1	45.9	48.8	3 -200	-39.9	EVACOL	
12:45	90.5	45.9	48.8	3 -200	-39.9		OPERATOR CYCLE STOP
12:45	91.2	46.0		7 -200			CYCLE CONTINUED
12:45	91.2	46.0		7 -200			
12:46	88.0	45.9		7 -200			
12:47	84.2	45.1		7 -200			
12:48	80.4	44.5		7 -200			
12:49	76.8	44.1		5 -200			
12:50	73.2	43.8		7 -200			
12:51	69.8	43.7		3 -200			
12:52	66.5	43.6		-200			
12:53	63.4	43.6		-200			
12:54	60.4	43.5		-200			
12:55	57.5	43.4		-200			
12:56	54.6	43.4		-200			
12:57	51.8	43.3		5 -200			
12:58	49.2	43.3		-200		ELIAGUATION EDECCHER	
12:59	48.4	43.3		-200		EVACUATION PRESSURE	
> 12:59	48.4	43.3				AFIER VA	CUUM HOLD=====
13:00	48.3	43.4		-200 -200			
13:00	48.3	43.4	30.1	200	-39.9		
MAX:	91.2	46.0	50.1	-200	-39.9	PHASE 0:14	PHASE ELAPSED 0:15
MIN:	48.3	43.3	48.6	5 0	0.1		CYCLE 1:49
			CAC TH	OTT 4 7	777 A 6777		
			GAS WA	ion A l	TOAGE		
13:00	48.3	43.4	50.2	-200	-39.9	======================================	1
13:01	54.2	44.7	50.4	-200	-39.9		
13:02	59.2	46.2	50.6	-200	-39.9		
13:03	64.2	47.1	50.9	-200	-39.9		
13:04	69.2	47.4	51.2	-200	-39.9		
13:05	74.2	47.6	51.4	-200	-39.9		
13:06	79.2	47.7		-200			
13:07	84.1	47.8	52.1	-200	-39.9		

DDI ANTARES KORSCP V3Q-1 07/11/19 Thu 13:08 CYCLE 27 CHECK VALUE 14543 STERILE LOT # STACK TEST 1

C23 & E FED	PRESS	TEMP (DEG C)	RH VAP % GAS		H20	AT ADMED O MEDGACES	ACUPTONI WALLENY
TIME	KPAA	AVG	% GAS	MG/L	MG/L	ALARMS & MESSAGES	ACTION TAKEN
13:08	89.2	47.8	52.4	-200	-39.9		
13:09	94.2	47.8			-39.9		
13:09	94.8	47.8	52.7	-200	-39.9	======= RELEASE HOLD	1
13:10	95.1	47.4	52.8	-200	-39.9		
13:10	95.1	47.4	52.8	-200	-39.9	====== EVACUATION	
13:11	92.0	46.5			-39.9		
13:12	88.1	45.2			-39.9		
13:12	87.7	45.1			-39.9	SLOW EVACUATION	
13:13	84.3	44.3			-39.9		
13:14	80.5	43.8			-39.9		
13:15	76.7	43.4			-39.9		
13:16	73.1	43.2			-39.9		
13:17 13:18	69.7 66.4	43.0 42.9			-39.9 -39.9		
13:16 13:19	63.2	42.9			-39.9		
13:19	60.2	42.8			-39.9		
13:21	57.2	42.8			-39.9		
13:22	54.3	42.8			-39.9		
13:23	51.5	42.7			-39.9		
13:24	48.8	42.6			-39.9		
13:24	48.4	42.6			-39.9	EVACUATION PRESSURE	
13:24	48.4	42.6			-39.9	======= VACUUM HOLD	Annual spaces which which the board about the board of th
13:25	48.3	42.8			-39.9		
13:25	48.3	42.8	54.0	-200	-39.9	======= RELEASE 2	and the state an
13:26	54.1	44.2	54.0	-200	-39.9		
13:27	59.0	45.8	53.9	-200	-39.9		
13:28	64.1	46.8	54.0	-200	-39.9		
13:29	69.0	47.2			-39.9		
13:30	74.0	47.4			-39.9		
13:31	79.1	47.5			-39.9		
13:32	84.1	47.5			-39.9		
13:33	89.1	47.6			-39.9		
13:34	94.1	47.6			-39.9		
13:34	94.8 95.0	47.6 47.2			-39.9 -39.9	======= RELEASE HOLD	
13:35 13:35	95.0	47.2			-39.9 -39.9	====== EVACUATION	2 ========
13:35	91.9	46.2			-39.9 -39.9	EVACONITON	<u> </u>
13:37	88.0	44.8			-39.9		
13:37	87.7	44.7			-39.9	SLOW EVACUATION	
13:38	84.1	43.9			-39.9		
13:39	80.3	43.3			-39.9		
13:40	76.5	42.9			-39.9		
13:41	72.8	42.7	53.9	-200	-39.9		
13:42	69.3	42.5	53.8	-200	-39.9		
13:43	66.0	42.4	53.7	-200	-39.9		
13:44	62.8	42.4			-39.9		
13:45	59.8	42.3	53.7				
13:46	56.8	42.3	53.7				
13:47	54.0	42.3	53.6				
13:48	51.2	42.3	53.6				
13:49	48.4	42.3			-39.9	TWACIIATION DECOME	
13:49 13:49	48.4 48.4	42.3 42.3			-39.9 -30 0	EVACUATION PRESSURE ====================================	
エン・マフ	70.7	~? L + J	JJ.J \	-200	32.3	VACOUM ROLD	

DDI ANTARES KORSCP V3Q-1 07/11/19 Thu 13:50 CYCLE 27 CHECK VALUE 14543 STERILE LOT # STACK TEST 1

TIME	PRESS KPAA	TEMP (DEG C) AVG	RH VAP ETO H2O % GAS MG/L MG/L	ALARMS & MESSAGES ACTION TAKEN
4.0	40.4	40.5	50 5 000 00 0	
13:50 13:50	48.4 48.4	42.5 42.5	53.5 -200 -39.9 53.5 -200 -39.9	======= RELEASE 3 ==========
		44.1	53.5 -200 -39.9	The state of the s
13:51	54.2		53.4 -200 -39.9	
13:52	59.2	45.9 46.8	53.4 -200 -39.9	
13:53 13:54	64.2 69.2	47.4	53.4 -200 -39.9	
13:55	74.2	47.6	53.3 -200 -39.9	
13:55 13:56	79.2	47.8	53.2 -200 -39.9	
13:57	84.2	47.9	53.2 -200 -39.9	
13:58	89.2	47.9	53.2 -200 -39.9	
13:59	94.1	47.9	53.2 -200 -39.9	
14:00	94.8	48.0	53.2 -200 -39.9	======= RELEASE HOLD 3 ========
14:01	94.9	47.6	53.2 -200 -39.9	KEDIKADI IKADI
14:01	94.9	47.6	53.2 -200 -39.9	====== EVACUATION 3 ========
14:02	91.8	46.7	53.1 -200 -39.9	TAINVOITION 2
14:03	87.8	45.3	53.0 -200 -39.9	
14:03	87.5	45.3	53.0 -200 -39.9	SLOW EVACUATION
14:04	83.9	44.4	53.0 -200 -39.9	DEGN EVILOUITION
14:05	80.1	43.8	53.0 -200 -39.9	
14:06	76.3	43.5	52.8 -200 -39.9	
14:07	72.6	43.3	52.8 -200 -39.9	
14:08	69.1	43.2	52.8 -200 -39.9	
14:09	65.8	43.2	52.7 -200 -39.9	
14:10	62.6	43.1	52.7 -200 -39.9	
14:11	59.5	43.1	52.7 -200 -39.9	
14:12	56.6	43.1	52.6 -200 -39.9	
14:13	53.7	43.1	52.6 -200 -39.9	
14:14	50.9	43.2	52.6 -200 -39.9	
14:15	48.4	43.1	52.5 -200 -39.9	EVACUATION PRESSURE
14:15	48.4	43.1	52.5 -200 -39.9	======= VACUUM HOLD 3 =========
14:16	48.4	43.3	52.5 -200 -39.9	
14:16	48.4	43.3	52.5 -200 -39.9	======= RELEASE 4 ============
14:17	54.2	44.9	52.4 -200 -39.9	
14:18	59.2	46.8	52.4 -200 -39.9	
14:19	64.2	47.7	52.3 -200 -39.9	
14:20	69.3	48.2	52.3 -200 -39.9	
14:21	74.2	48.5	52.2 -200 -39.9	
14:22	79.2	48.6	52.2 -200 -39.9	
14:23	84.1	48.6	52.2 -200 -39.9	
14:24	89.2	48.6	52.1 -200 -39.9	
14:25	94.2	48.6	52.1 -200 -39.9	
14:25	94.8	48.6	52.1 -200 -39.9	======= RELEASE HOLD 4 ========
14:26	95.0	48.3	52.1 -200 -39.9	
14:26	95.0	48.3	52.1 -200 -39.9	======= EVACUATION 4 =========
14:27	91.9	47.3	52.1 -200 -39.9	
14:28	87.8	45.9	52.0 -200 -39.9	
14:28	87.4	45.8	52.0 -200 -39.9	SLOW EVACUATION
14:29	83.8	44.9	51.9 -200 -39.9	
14:30	80.0	44.2	51.9 -200 -39.9	
14:31	76.1	43.9	51.8 -200 -39.9	
14:32	72.5	43.6	51.8 -200 -39.9	
14:33	68.9	43.5	51.7 -200 -39.9	

DDI ANTARES KORSCP V3Q-1 07/11/19 Thu 14:34 CYCLE 27 CHECK VALUE 14543 STERILE LOT # STACK TEST 1

TIME	PRESS KPAA	TEMP (DEG C) AVG	RH VAP ETO H2O % GAS MG/L MG/L	ALARMS & MESSAGES ACTION TAKEN
AL ISS A SECOND	444 44 4		70 01.15 1.207.15 1.207.15	TREES OF PRIODICION TRACES
14:34	65.6	43.5	51.8 -200 -39.9	
14:35	62.5	43.5	51.8 -200 -39.9	
14:36	59.3	43.5	51.9 -200 -39.9	
14:37	56.3	43.5	52.0 -200 -39.9	
14:38	53.4	43.5	52.1 -200 -39.9	
14:39	50.6	43.5	52.3 -200 -39.9	
14:40	48.4	43.4	52.4 -200 -39.9	EVACUATION PRESSURE
14:40	48.4	43.4	52.4 -200 -39.9	======= VACUUM HOLD 4 ========
14:41	48.4	43.6	52.5 -200 -39.9	
14:41	48.4	43.6	52.5 -200 -39.9	
MAX:	95.1	48.6	54.1 -200 -39.9	PHASE 1:40 PHASE ELAPSED 1:40
MIN:	48.3	42.3	50.2 0 0.1	CYCLE 3:29
			RELEASE PHASE	
14:41	48.4	43.6	52.5 -200 -39.9	
14:41	48.4	43.6	52.5 -200 -39.9	LOOSEN DOOR LOCKS
14:42	53.4	45.1	52.7 -200 -39.9	
14:43	58.0	46.9	52.8 -200 -39.9	
14:43	58.4	47.0	52.8 -200 -39.9	SLOW INJECTION
14:44	62.3	47.8	52.8 -200 -39.9	
14:45	66.3	48.2	52.9 -200 -39.9	
14:46	70.1	48.3	52.9 -200 -39.9	
14:47	73.7	48.3	53.0 -200 -39.9	
14:48	77.0	48.2	52.9 -200 -39.9	
14:49	80.0	48.1	53.0 -200 -39.9	
14:50	82.8	48.0	53.0 -200 -39.9	
14:51	85.3	47.9	53.0 -200 -39.9	
14:52	87.6	47.7	53.1 -200 -39.9	
14:53	89.7	47.6	53.1 -200 -39.9	
14:54	91.5	47.5	53.1 -200 -39.9	
14:55	93.2	47.4	53.1 -200 -39.9	
14:56	94.6	47.3	53.2 -200 -39.9	
14:57	95.9	47.3	53.1 -200 -39.9	
14:58	96.9	47.2	53.0 -200 -39.9	
14:59	97.7	47.0	53.1 -200 -39.9	
14:59	98.0	47.0	53.1 -200 -39.9	
MAX:	98.0	48.3	53.2 -200 -39.9	PHASE 0:18 PHASE ELAPSED 0:18
MIN:	48.4	43.6	52.5 0 0.1	CYCLE 3:48

DDI ANTAI STERILE I		SCP V3Q-1 ( STACK TEST 1	07/11/19 Th	u 14:59	CYCLE	27	CHECK VALUE 1454	13
TIME	PRESS KPAA	TEMP (DEG C) AVG	RH VAP E % GAS M		ALARMS & MESS	SAGES	ACTION TAKEN	
			CYCLE CO	MPLETE PHA	SE			
14:59					TOTAL CYCLE	3:47	CYCLE ELAPSED	3:48
			SIGNATUR	ES:		····	OPERATOR	
							SUPERVISOR	

Test 3

EO STERILIZER #1 LONG ISLAND STERILIZATION 175 WIRELESS BLVD. HAUPPAUGE, NY 11788 T: 1.631.435.4815

RUN 3

DATE 07/11/19 Thu PROG VERSION KORSCP V3Q-1

STACK TEST 3

STERILANT EO CHECK VALUE 14543

OPERATOR

REK

CYL STRAT WI CYL END WI 45.8 ETO USED WT

STERILE LOT #

STERILANT TANK LOT # 190606E000241, TARE WEIGHT: 274.0 LBS

PROCESS PARAMETERS

CYCLE 27

CHAMBER TEMP 46 C, BLOWER IS USED

VACUUM A 48.4 KPAA, 6.4 KPA/MIN

NITROGEN DILUTION 2 CYCLES: NITROGEN: 98.0 KPAA, 5.0 KPA/MIN

EVAC: 48.4 KPAA, 6.4 KPA/MIN

INJ: 75.4 KPAA, 2.0 KPA/MIN, EO, LGT 20 C GAS A 1 CYCLES:

90.0 KPAA, 2.0 KPA/MIN, SECOND NITROGEN

GAS DWELL 90.0 KPAA, -1.0 KPA, DWELL 0:10 HH:MM, MAKEUPS: N2

AFTER VACUUM 48.4 KPAA, 6.4 KPA/MIN, HOLD 0:01 HH:MM

GAS WASH A 4 CYCLES; RLS: 94.8 KPAA, 5.0 KPA/MIN, HOLD 0:01 HH:MM, NITR

VAC: 48.4 KPAA, 6.4 KPA/MIN, HOLD 0:01 HH:MM

RELEASE 98.0 KPAA, 7.0 KPA/MIN

PRESS TEMP (DEG C) RH VAP ETO H2O

AVG 8 TIME KPAA GAS MG/L MG/L ALARMS & MESSAGES ACTION TAKEN

14:47 EXISTING HIDI OVERRIDES:

BlwrOK to MAN ON ExhVlv to MAN OFF Blower to MAN ON

# VACUUM A PHASE

14:47	97.1	46.7	33.6 -200 -39.9	
14:48	93.3	46.4	33.6 -200 -39.9	
14:49	88.3	45.0	33.6 -200 -39.9	
14:49	87.9	44.9	33.6 -200 -39.9	SLOW EVACUATION
14:50	83.7	44.3	33.6 -200 -39.9	
14:51	79.2	43.8	33.6 -200 -39.9	
14:52	74.9	43.5	33.6 -200 -39.9	
14:53	70.8	43.3	33.6 -200 -39.9	
14:54	66.8	43.2	33.6 -200 -39.9	
14:55	62.9	43.1	33.6 -200 -39.9	
14:56	59.1	43.0	33.6 -200 -39.9	
14:57	55.5	42.8	33.6 -200 -39.9	
14:58	52.2	42.8	33.6 -200 -39.9	
14:59	48.8	42.8	33.6 -200 -39.9	

DDI ANTARES KORSCP V3Q-1 07/11/19 Thu 14:59 CYCLE 27 CHECK VALUE 14543 STERILE LOT # STACK TEST 3 PRESS TEMP (DEG C) RH VAP ETO H20 KPAA AVG % GAS MG/L MG/L ALARMS & MESSAGES ACTION TAKEN TIME 14:59 48.4 42.7 33.6 -200 -39.9 MAX: 97.1 46.7 33.6 -200 -39.9 PHASE 0:12 PHASE ELAPSED 0:12MIN: 48.4 42.7 33.6 0 0.1 CYCLE 0:12 NITROGEN DILUTION PHASE

	DDI ANTAE STERILE I		CP V3Q-1 0 STACK TEST 3	7/11/19 T	'hu	15:40	C	YCLE	27	CHECK	VALUE	14543
	TIME	PRESS KPAA	TEMP (DEG C) AVG	RH VAP % GAS		H2O MG/L	ALARMS	s & Mess	BAGES	AC	TION TA	IKEN
	15:40	59.3	42.7			-39.9						
	15:41 15:42	55.8 52.4	42.6 42.5			-39.9						
		48.9	42.5 42.5			-39.9 -39.9						
		48.4	42.5			-39.9						
	MAX:	98.0	48.9	33.8	-200	-39.9		PHASE	0:43	PHASE	ELAPSE	D 0:43
	MIN:	48.3	42.5	33.6	0	0.1					CYCL	
				GAS A (	EO) 1	PHASE	Ad d	ETO				
<del></del>	15:43	48.4	42.5	33 S	200	-39.9			ERILAN	п 1.		
·	15:44	50.6	43.0	33.8					LIBRA LIMIN.	L <u>1</u> .		
	15:45	52.6	44.7			-39.9						
	15:46	54.5	45.9			-39.9						
	15:47 15:48	56.5 58.4	46.6 47.0			-39.9 -39.9						
	15:49	60.4	47.0			-39.9						
	15:50	62.4	46.9			-39.9						
	15:51	64.3	46.9			-39.9						
	15:52	66.4	47.0			-39.9						
	15:53 15:54	68.3 70.3	47.0 46.9			-39.9 -39.9						
	15.54	70.5	46.9			-39.9 -39.9	SLOW I	NJECTIO	M			
	15:55	72.3	46.9			-39.9						
	15:56	74.2	46.9			-39.9						
$\rightarrow$		75.4 77.5	46.9			-39.9	***************************************	==== SE	ECOND NI	TROGEN	1 =	
		79.6	47.1 47.0			-39.9 -39.9						
	16:00	81.6	47.1			-39.9						
	16:01	83.6	47.0			-39.9						
	16:02	85.6	47.0	33.9								
	16:03 16:04	87.6 89.6	47.0 47.0	33.9 - 33.9 -								
	16:04	90.0	47.0			-39.9						
	MAX:	90.0	47.1	33.9 -	-200	-39.9		PHASE	0:20	PHASE	ELAPSE	D 0:20
	MIN:	48.4	42.5	33.8					* • = *		CYCL	
		ESTIMAT	'ED STERILANT U	JSED THIS	PHAS	Œ:	45.9,	CYCLE	TOTAL:	45.9		
				GAS DWEI	TJ. (T	O) PHA	SR					
	16.04	00 4	47 A		-		<del></del>					
	16:04 16:05	90.1 90.2	47.0 46.8	33.9 - 34.0 -								
	16:06	90.2	46.6	34.0 -								
	16:07	90.2	46.4	34.0 -	-200	-39.9						
	16:08	90.2	46.3	34.0 -								
	16:09 16:10	90.2 90.2	46.3 46.2	34.0 - 34.0 -								
	TO + TO	30.4	20.2	J4.U -	- <u>~</u> UU	-33.3						

DDI ANTAR STERILE L		CP V3Q-1 0 STACK TEST 3	7/11/19 Thu 16:11	CYCLE 27	CHECK VALUE 14543
TIME	PRESS KPAA	TEMP (DEG C) AVG	RH VAP ETO H2O % GAS MG/L MG/L	ALARMS & MESSAGES	ACTION TAKEN
16:11 16:12 16:13 16:14 16:14	90.2 90.2 90.2 90.2 90.2	46.2 46.2 46.2 46.2 46.2	34.0 -200 -39.9 34.0 -200 -39.9 34.0 -200 -39.9 34.0 -200 -39.9 34.0 -200 -39.9		
MAX: MIN:	90.2 90.0	47.0 46.2	34.0 -200 -39.9 33.9 0 0.1	PHASE 0:10	PHASE ELAPSED 0:10 CYCLE 1:26
			AFTER VACUUM PHASE		
16:17 16:18 16:19 16:20 16:21 16:22 16:23 16:24 16:24 16:24 16:25 16:25	90.2 86.6 81.5 76.8 72.4 68.4 64.5 60.8 57.2 53.8 50.5 48.4 48.4	46.2 46.1 45.0 44.2 43.9 43.6 43.5 43.5 43.3 43.3 43.3 43.5	34.0 -200 -39.9 34.0 -200 -39.9 34.0 -200 -39.9 34.0 -200 -39.9 34.0 -200 -39.9 34.0 -200 -39.9 34.1 -200 -39.9		CUUM HOLD========
MAX: MIN:	90.2 48.4	46.2 43.3	34.1 -200 -39.9 34.0 0 0.1	PHASE 0:11	PHASE ELAPSED 0:11 CYCLE 1:38
			GAS WASH A PHASE		
16:25 16:26 16:27 16:28 16:29 16:30	48.4 53.6 58.7 63.7 68.7 73.7	43.5 45.1 46.6 47.5 48.0 48.2	34.1 -200 -39.9 34.1 -200 -39.9 34.1 -200 -39.9 34.1 -200 -39.9 34.1 -200 -39.9 34.1 -200 -39.9	======= RELEASE	1

ISO 9001:2015

Certifed By

UL DQS

10001297 QM15

# Certificate of Calibration "

TEST #81206-601

ITEM # 63039

ISSUED BY

MCS Calibration, Inc.

LOCATION: 175 WIRELESS BLVD
STERILIZATION ROOM

1533 LINCOLN AVENUE HOLBROOK, NEW YORK 11741 (631) 471-6900 FAX (631) 471-6902

CUSTOMER LONG ISLAND STERILIZATION DESCRIPTION SCALE / PLATFORM / DIGITAL MFR. FAIRBANKS

> MODEL H90-3051 RANGE 0-800 X 0.1 lbs

Calibration Date 12/6/2018 Calibration Due 12/6/2019

PO # L55244 S/N H359735FE ID # STERILIZER #1

This certificate was prepared by MCS Calibration, Inc. in compliance with MIL-STD-45662A, ANSI/NCSL Z540 & ISO 9001. This instrument was calibrated using test equipment whose accuracy is traceable through the NATIONAL INSTITUTE of STANDARDS and TECHNOLOGY or accepted values of natural physical constants, to the International System of Units(SI units). This instrument has been added to the MCS RECALIBRATION PROGRAM. This certificate will not be reproduced except in full.

POUNDS ACTUAL 0 100 200 300 400 500 600 700 800

REQUIRED ACCURACY: +/- 1 LB

SERVICE NOTE: THIS UNIT MEETS THE REQUIRED ACCURACY, "AS FOUND, AS LEFT"

**ENVIRONMENTAL CONDITIONS** 

Quality Manual Rev. 24

PROCEDURE MCS2009 rev. 03

72 DEG F

30 % RH

MCS TRACEABILITY

12 BY WT

MCS ITEM # 8669 EQUIPMENT USED
WEIGHTS/STEEL

TRACEABILITY #

**CURRENTLY DUE** 

71025-Z01

10/25/2020

Q.A. MCS

Kenneth Ja Ma

VALID ONLY WHEN APPROVED BY MCS QUALITY ASSURANCE PERSONNEL

PG 1 of 1

ISO 9001:2015 Certifed By **UL DQS** 10001297 QM15

# Certificate of Calibration '

TEST #81206-603

ITEM # 63040

MCS Calibration, Inc.

LOCATION: 175 WIRELESS BLVD STERILIZATION ROOM

1533 LINCOLN AVENUE HOLBROOK, NEW YORK 11741 (631) 471-6900 FAX (631) 471-6902

CUSTOMER LONG ISLAND STERILIZATION DESCRIPTION SCALE / PLATFORM / DIGITAL MFR. FAIRBANKS

MODEL FB350 RANGE 0-800 X 0.1 lbs Calibration Date 12/6/2018 Calibration Due 12/6/2019

PO # L55244

S/N H359730FE / 999994 ID# STERILIZER#2

This certificate was prepared by MCS Calibration, Inc. in compliance with MIL-STD-45662A, ANSI/NCSL Z540 & ISO 9001. This instrument was calibrated using test equipment whose accuracy is traceable through the NATIONAL INSTITUTE of STANDARDS and TECHNOLOGY or accepted values of natural physical constants, to the International System of Units(SI units). This instrument has been added to the MCS RECALIBRATION PROGRAM. This certificate will not be reproduced except in full.

		TEST DATA
POUNDS ACTUAL	POUNDS READS	
0.0	0.0	
100	99.8	
200	199.8	
300	299.6	A CETATAR CROSS
400	399.8	ACCEPTED
500	499.4	11 1/2
600	599.4	Name   12- 21 18
700	699.4	Name Date
800	799.4	Name   1-7-18

REQUIRED ACCURACY: +/- 1 LB

SERVICE NOTE: THIS UNIT MEETS THE REQUIRED ACCURACY, "AS FOUND, AS LEFT"

**ENVIRONMENTAL CONDITIONS** 

Quality Manual Rev. 24

PROCEDURE MCS2009 rev. 03

72 DEG F 30 % RH

MCS TRACEABILITY

12 BY WT

MCS ITEM #

**EQUIPMENT USED** 

TRACEABILITY #

**CURRENTLY DUE** 

8669

WEIGHTS / STEEL

71025-Z01

10/25/2020

Q.A. MCS

Kenneth In Ma

VALID ONLY WHEN APPROVED BY MCS QUALITY ASSURANCE PERSONNEL

PG 1 of 1

# DAMAS TANK SCRUBBER UNIT

DATE	TIME	PH	TEMP.	LQ.LEVEL	ВҮ	COMMENTS
7-11-19	6:30	-0.2	54°F	46	R.IC	1/4
7-11-19	Į.	-0.2	54°F	46	R.K	NA
7-11-19	7:30	-0.2	5 5 OF	46	PIK	NA
7-11-19	8:00	-0,2	55°F	46	R-K	~14
7-11-18	8:30	-0.2	5505	46	R.K	NA
7-11-19	9:00	-0.3	6100	46	P.K	NA
7-11-19	9:30	-0.3	640F	46	BK	2/4
7-11-19	10:00	-0.3	6700	46	RK	2/4
7-11-19	10:30	-0.3	67°F	46	RK	NA
7-11-19	11:00	-0.3	65-2	46	RK	2/1
7-11-19	11:30	-0-3	64 °F	46	RIT	NI
7-11-19	12:00	~0~)	6401	46	RIT	nld
7-11-19	12:30	-0-3	6401	46	RK	N/A
7-11-19	13700	-0-4	7101	46	RIS	NA
7-11-19	13:30	-0.4	7100	46	RK	NI
7-11-19	24:00	-0.4	2100	46	×15	n/f
7-11-19	14:30	-0.4	6801	46	RK	2/4
7-11-19	15:00	-0.4	68°F	46	RK	nly
7-11-15	15:30	-0.4	660F	46	RIS	NH
7-11-19	16:00	-0.4	6301	46	RK	NA
	16:30	-0.4	6501=	46	RIT	rly
7-11-19	17:00	NA	v (A	NA	1/1	NA